

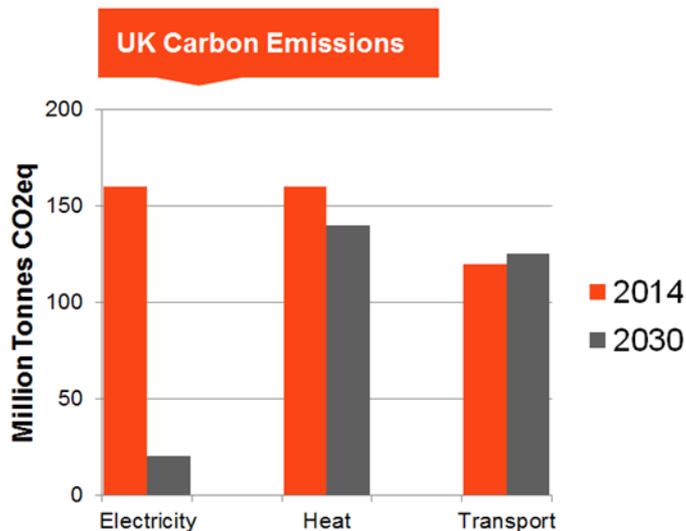
# Recent advances in gasification for waste-to-fuel applications

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# The UK Fuel Networks role in a 2050 whole energy system



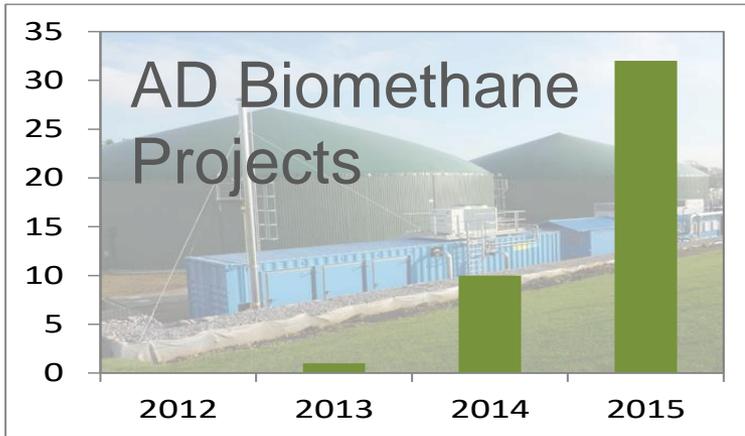
'2050 Energy Scenarios The UK Gas Networks role in a 2050 whole energy system' KPMG (2016)

'Future of Gas' National Grid (2016)

- ✓ We need low carbon, secure and affordable solutions for heat and transport (HGV, Aviation, Shipping)
- ✓ In its recent report, the CCC acknowledged that the UK has made good progress decarbonising the power sector, but '*almost no progress in the rest of the economy*'
- ✓ Sustainable drop-in fuels provide the lowest cost pathways to decarbonised heat and transport using existing infrastructure
- ✓ Feedstock should be cheap, abundant and not compete with land for food production



# Renewable Gas – Practical Decarbonisation



- Anaerobic Digestion: important role, but limited by feedstock type & availability
- BioSNG offers the potential to exploit a much wider range of feedstocks



## The BioSNG process



Feedstock

Syngas Production & Conditioning

Methanation

Refining

# The evolution towards BioSNG

## Dakota

The largest SNG facility in the world, with 3GWth input capacity (producing ~200,000 Nm<sup>3</sup>/hr CH<sub>4</sub>), fuelled by lignite. Gasifiers: Lurgi Dry Ash with Rectisol gas cleaning. Has Carbon capture fitted.



## GobiGas



Fuel: Wood pellets. Indirect gasifier. Phase 1: 32MWth input, Technology: Repotec

## Edmonton



Fuel: MSW. Steam-Oxy gasifier. Scale: 100k tonnes/year input, Technology: Enerkem

Waste-to-Alcohols

Biomass-to-Gas

Power to Gas

Coke oven gas (CO<sub>2</sub> meth.)

Coal-to-Gas

Methanation for gas cleaning (Ammonia synthesis, Hydrogen production, PEM fuel cells, etc.)

1902  
Sabatier

1910  
Haber-Bosch  
patent

1925  
Fischer-Tropsche

1950

1973  
Oil crises

2000

2014

2018  
Waste pilot

# The evolution towards BioSNG

## FEEDSTOCK

- The UK's dominant biomass resource is waste derived.
- Globally no BioSNG projects using waste feedstock



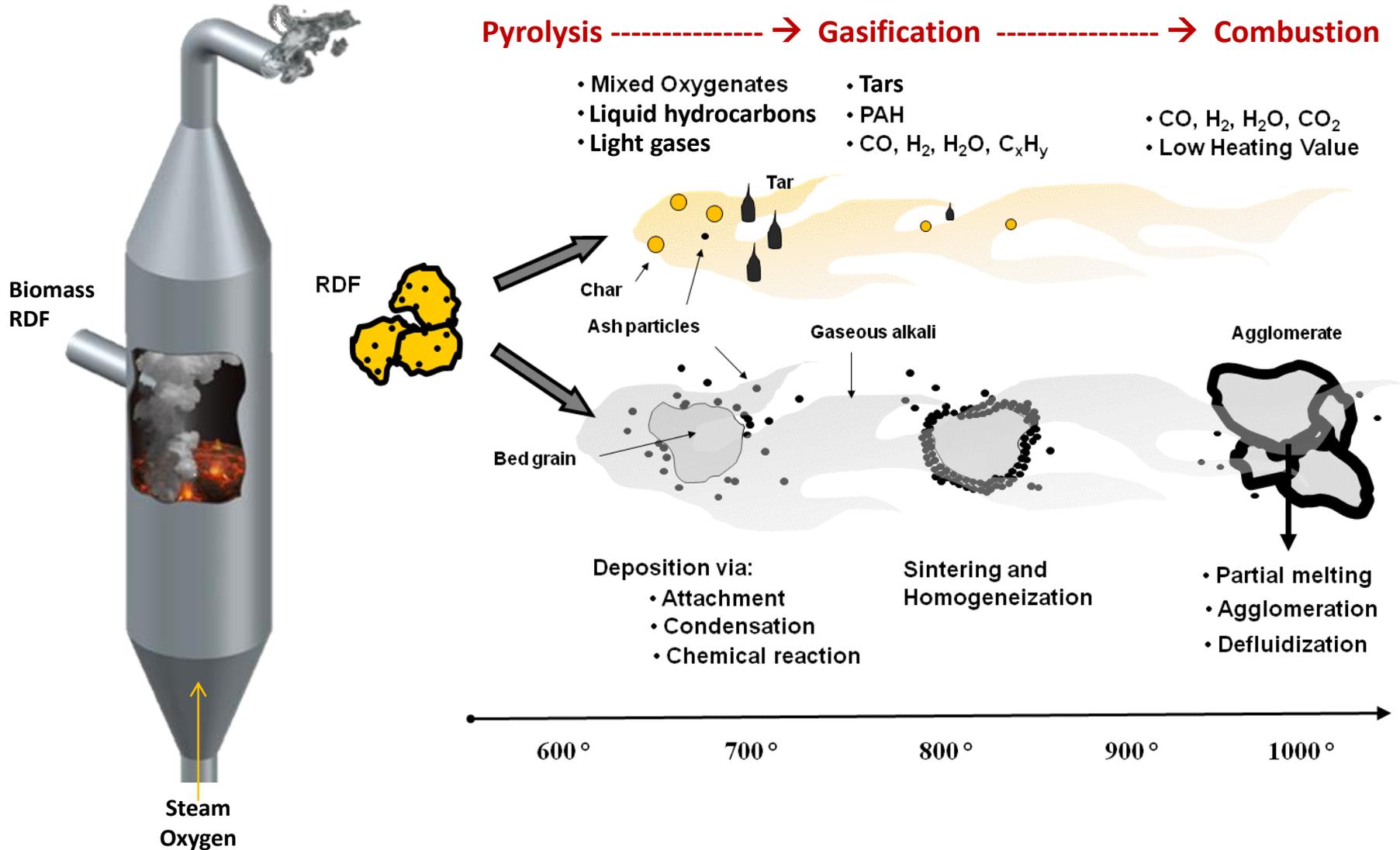
## TECHNICAL CHALLENGES

- Heterogeneous feedstock (size and composition)
- Sensitivity to ash content (quantity and composition)
- Tar yield
- Provision of clean, high quality synthesis gas
- Gas cleaning and Catalytic transformation at moderate scale, implicit in renewable resources

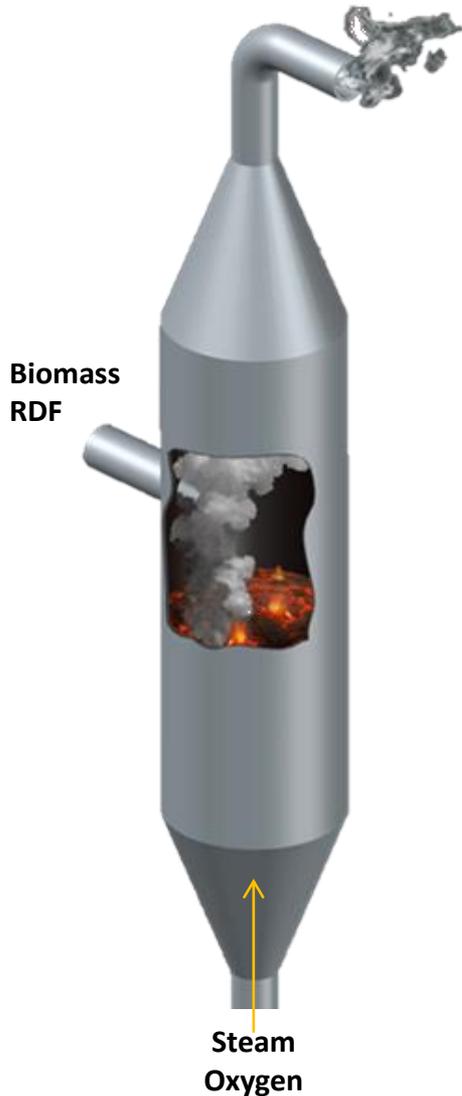
## DEVELOPMENT PATHWAY

- The technical approach needs piloting and sustained operation
- R&D efforts on new technologies

# The gasification step



# The gasification step



- Gasification by oxygen and steam
- Suited to non-homogeneous feedstocks
- Readily scalable
- No need for fuel pellettization/torrefaction
- Typically operate at 700-850°C

## Challenges with operation on waste

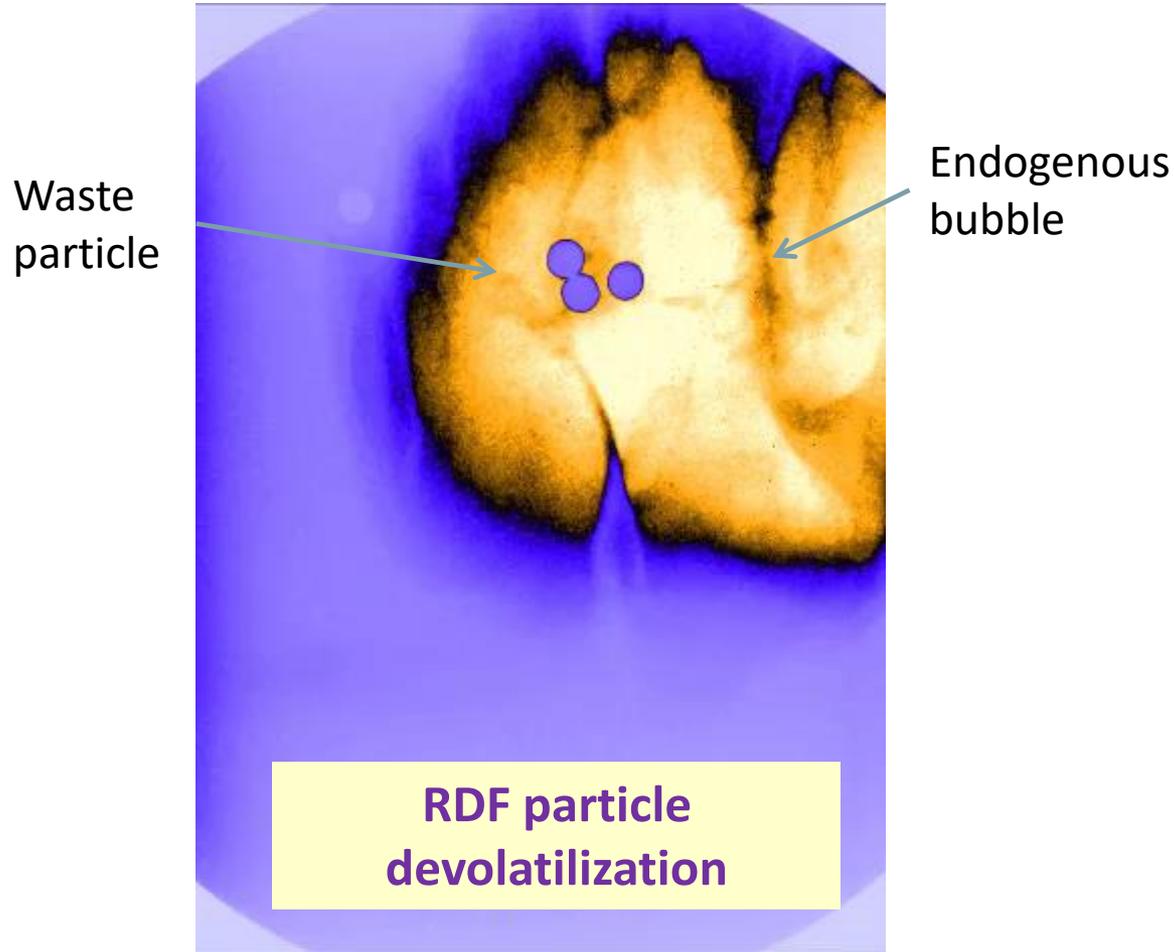
- Agglomeration risk (defluidization)
- > 100-10,000 mg/Nm<sup>3</sup> tar content
- > 5-10 g/m<sup>3</sup> VOC, C<sub><6</sub>H<sub>x</sub>
- > 5-10 ppmv organic sulphur
- Increase rates of ash deposition in the ducts and on heat transfer surfaces



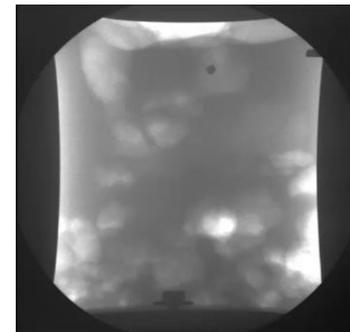
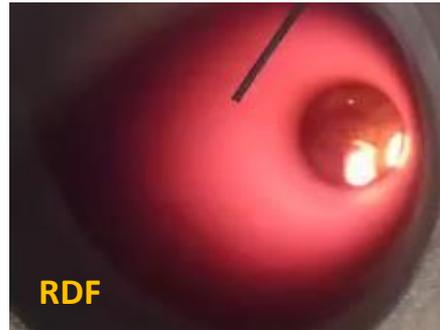
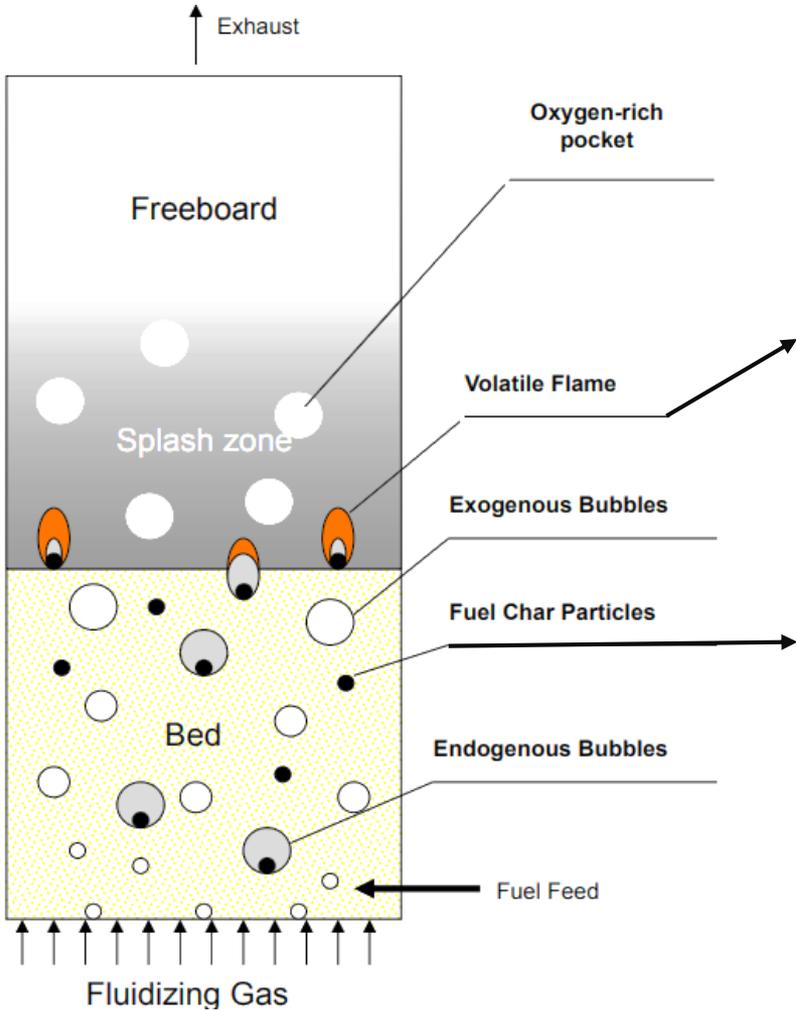
Ravenna (Italy) 200t/day  
RDF Fluidised Bed Plant



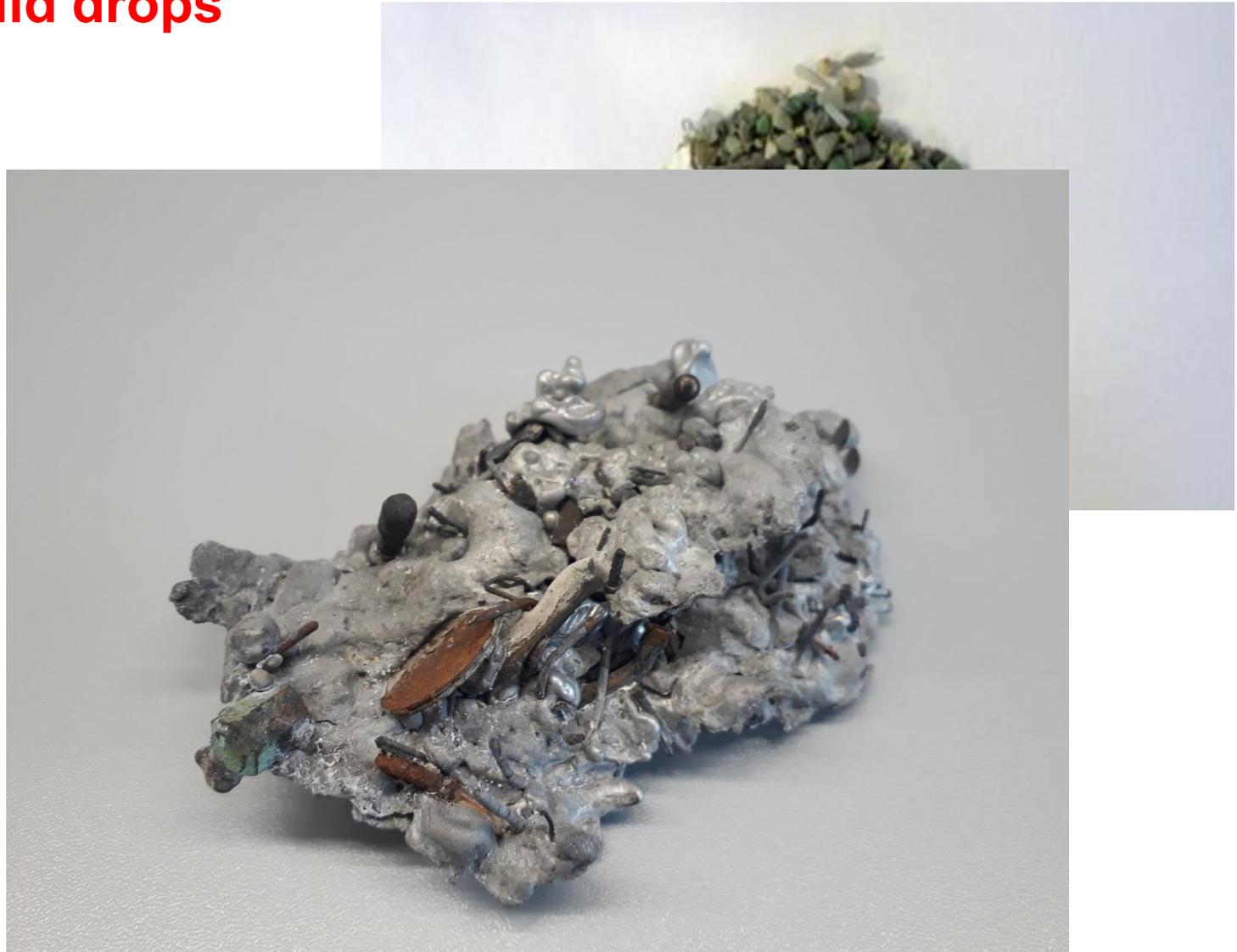
# X-Ray analysis of FBG at UCL



# Enhanced segregation from RDF...



... and solid drops

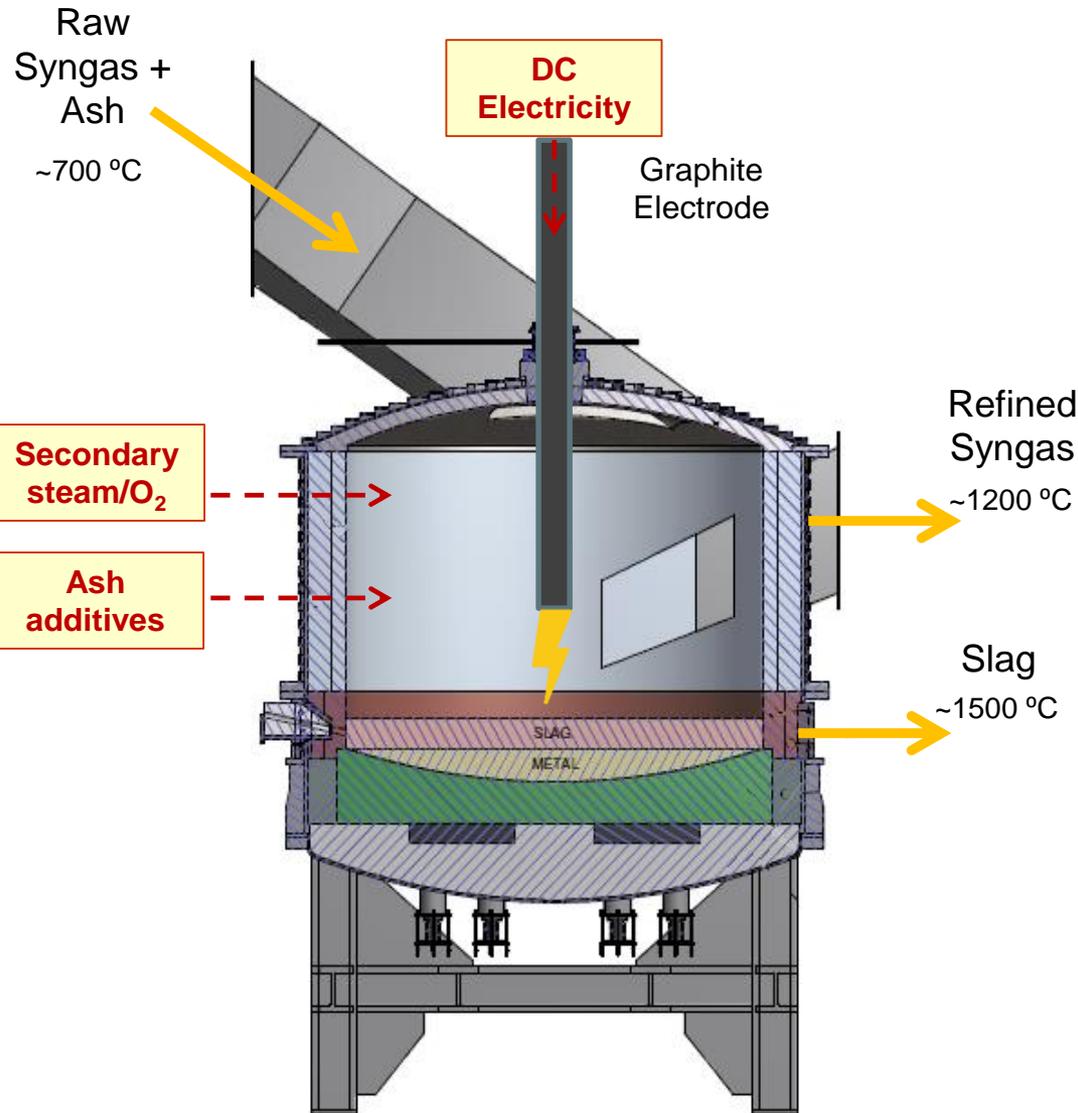


## Plasma assisted gasification: a multi-disciplinary and multiphysics problem

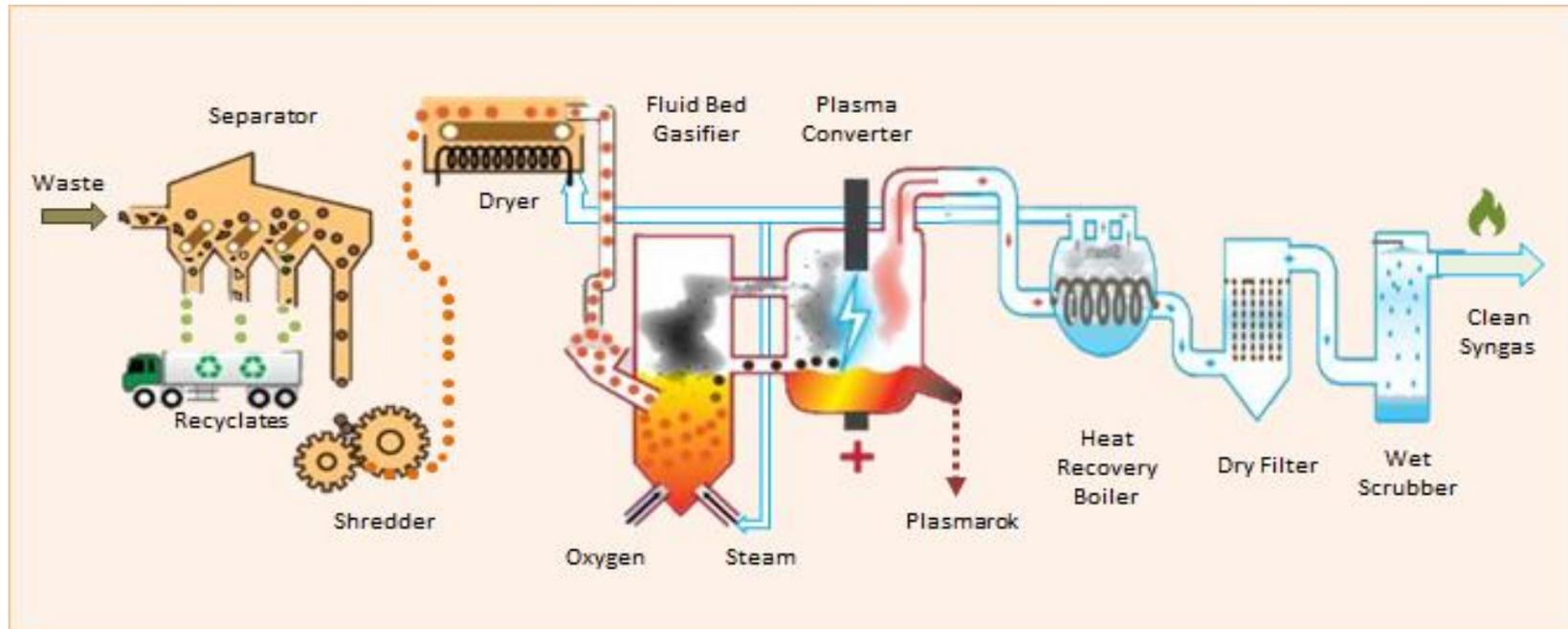
- Formed by DC or AC electric arcs, radio-frequency or microwave electromagnetic fields
- Highly ionised (typically 100%, at least 5%)
- Strong radiative emission
- Local  $T_{\text{gas}} = 2,000\text{-}20,000\text{K}$  (close to equilibrium)
- Highly electron density ( $\sim 10^{23} \text{ m}^{-3}$ )
- Very widely used in manufacturing and other industries (ash smelting, metal recovery, etc.)
- Quick start-up, possibility to couple with renewable electricity



# Thermal plasma reforming in DT furnaces



## The plasma-assisted gasification process



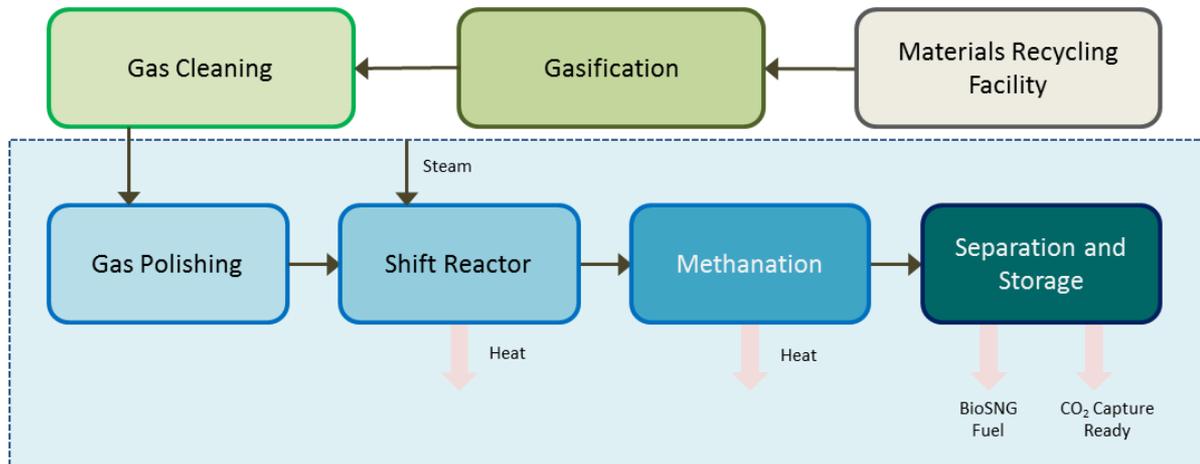
- Tars are converted overwhelmingly to CO and H<sub>2</sub>
- Organic-S is less than 500 ppbv, i.e. ~ 93% less than that of a conventional FBG gasifier
- **Ash is collected mostly as inert material**
- **Carbon to carbon conversion efficiency >96%**

## *The Pilot Plant*

# BioSNG PILOT PLANT (50 kWth)

## Project

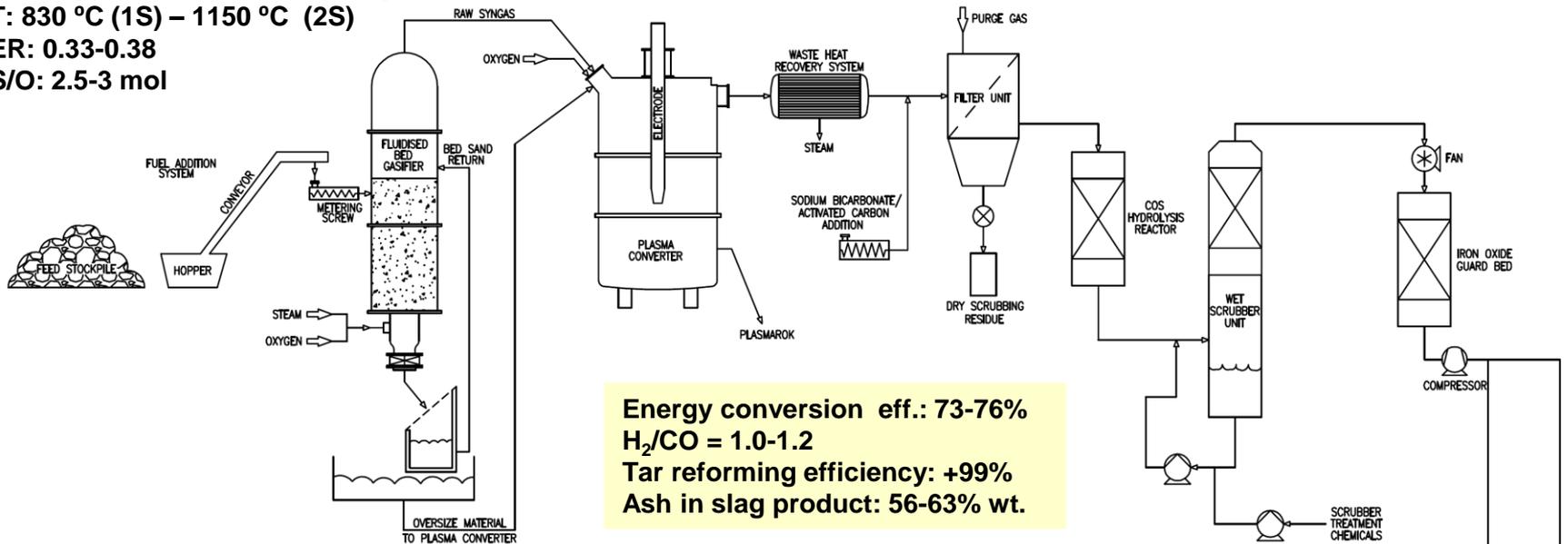
- ✔ Three year programme to establish technical, environmental and commercial viability of BioSNG production from waste and residues.
- ✔ Successfully completed March 2017.
- ✔ Overall cost £5m (£4m EU and UK grants).



# Pilot plant configuration

~100 kg/h RDF (GCV:22.1 MJ/kg)  
 T: 830 °C (1S) – 1150 °C (2S)  
 ER: 0.33-0.38  
 S/O: 2.5-3 mol

## Gasification plant

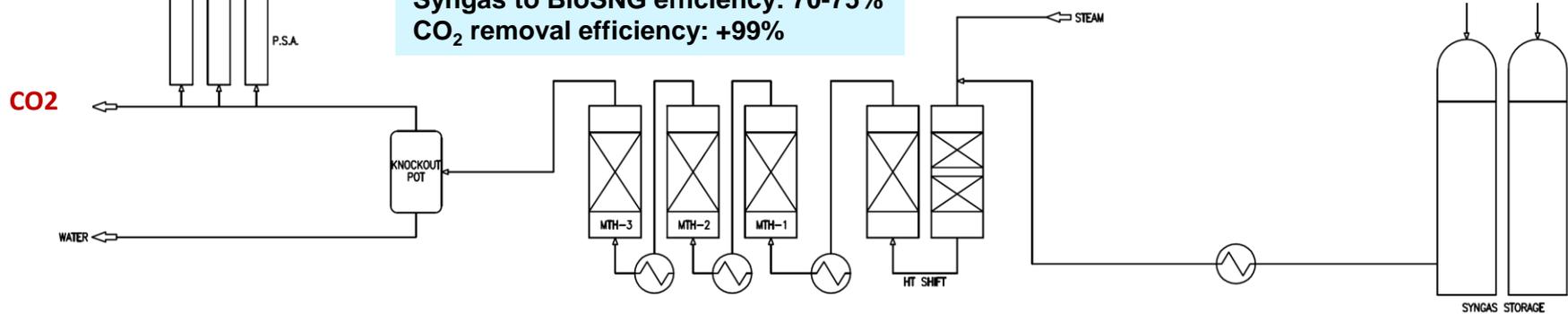


Energy conversion eff.: 73-76%  
 $H_2/CO = 1.0-1.2$   
 Tar reforming efficiency: +99%  
 Ash in slag product: 56-63% wt.

## BioSNG

Syngas in: 10-20 kg/h  
 Syngas to BioSNG efficiency: 70-75%  
 CO<sub>2</sub> removal efficiency: +99%

## BioSNG plant



# Feedstock



RDF (Refuse Derived Fuel)

Description:		RDF (as received)
Proximate analysis, % (w/w)		
	Fixed carbon	6.4
	Volatile matter	59.6
	Ash	19.1
	Moisture	14.9
Ultimate analysis, % (w/w)		
	C	41.0
	H	5.7
	O	17.5
	N	1.2
	S	0.2
	Cl	0.4
GCV, MJ/kg (dry basis)		22.1

ROC: > **60% wt. biomass content** in the feedstock

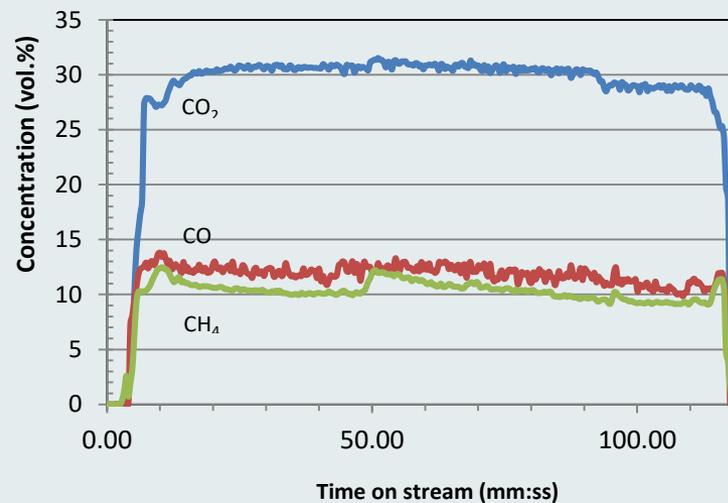
Category	Design Point	Lower limit	Upper limit
Paper (wt%)	30.36	19.47	64.00
Plastic Film (wt%)	5.72	3.55	17.80
Dense Plastics (wt%)	8.38	5.50	16.20
Textiles (wt%)	3.64	0.20	8.17
Disposable Nappies (wt%)	4.91	0.00	8.00
Misc Combustible (wt%)	6.40	2.29	10.92
Misc Non-Combustible (wt%)	6.08	0.00	8.93
Glass (wt%)	7.01	0.60	11.00
Putrescible (wt%)	16.82	3.00	27.00
Ferrous (wt%)	6.61	1.10	11.69
Non-ferrous (wt%)	1.96	0.60	2.90
Fines (wt%)	2.13	1.00	5.50
Total	100.00		
CV (MJ/kg)	10.05	9.08	13.62
RDF biomass content (wt%)	67.7	49.1	80.1
RDF biomass content (energy%)	64.1	39.9	79.8

## Syngas quality

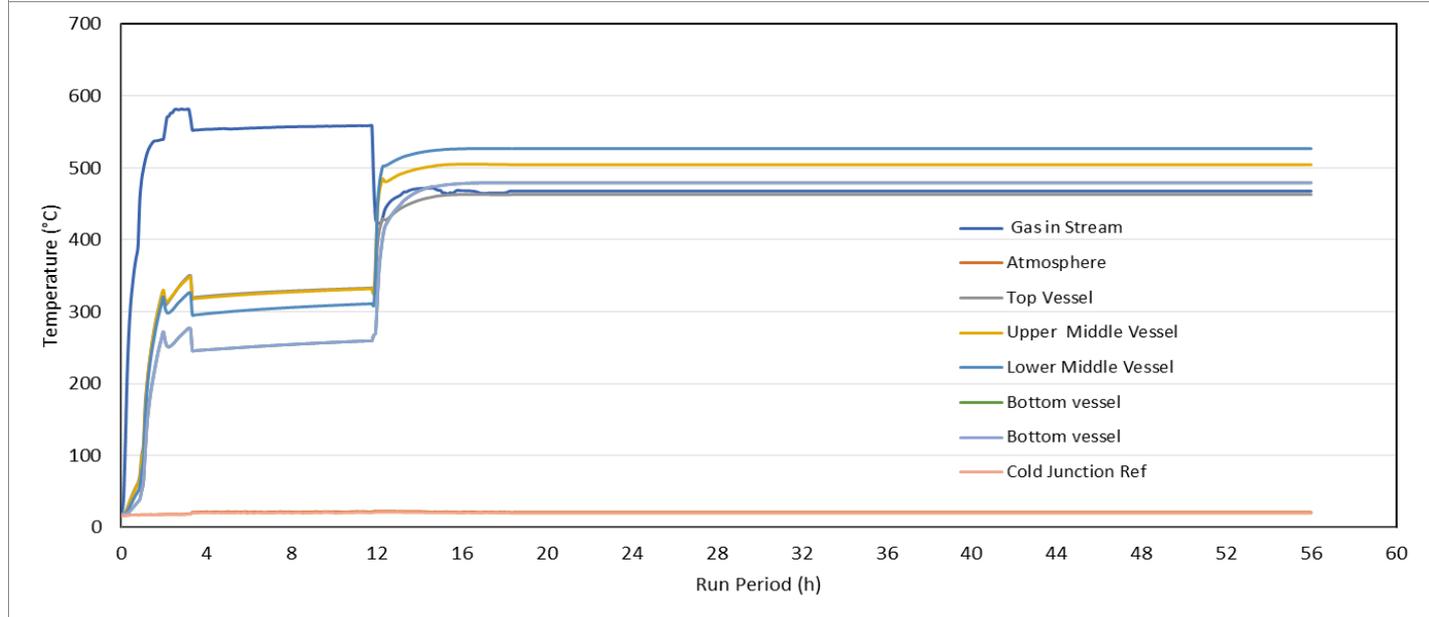
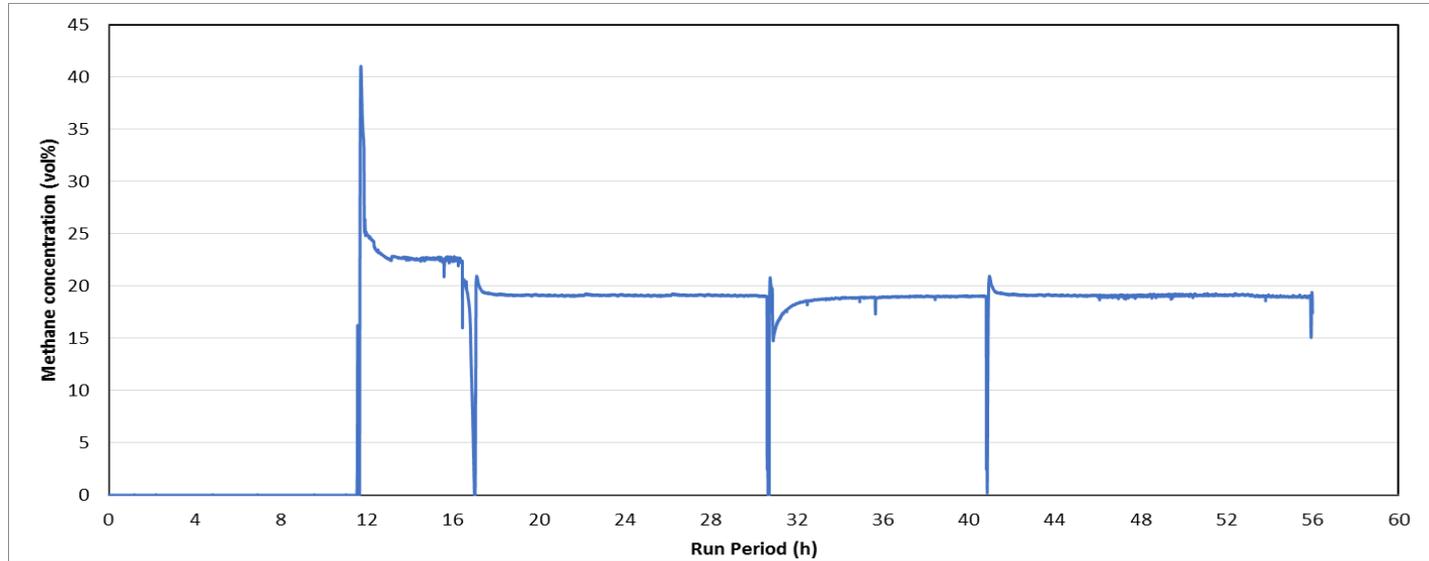
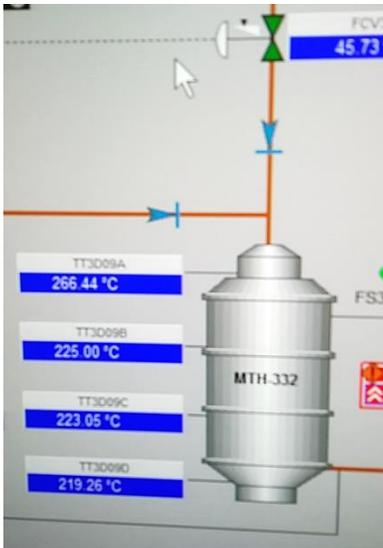


Quality Parameter:		Stored syngas
<b>Composition:</b>		
H <sub>2</sub>	vol.%	35.77
CO	vol.%	33.20
CO <sub>2</sub>	vol.%	23.54
CH <sub>4</sub>	vol.%	1.67
H <sub>2</sub> O	vol.%	0.89
Other	vol.%	4.90
<b>Energy Analysis</b>		
NCV	MJ/kg	8.75

## Methanation trials

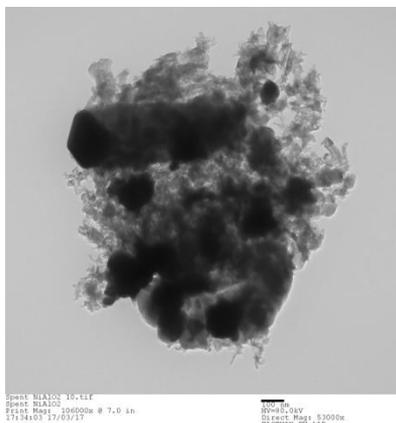


# 4-day methanation with waste-derived syngas ...

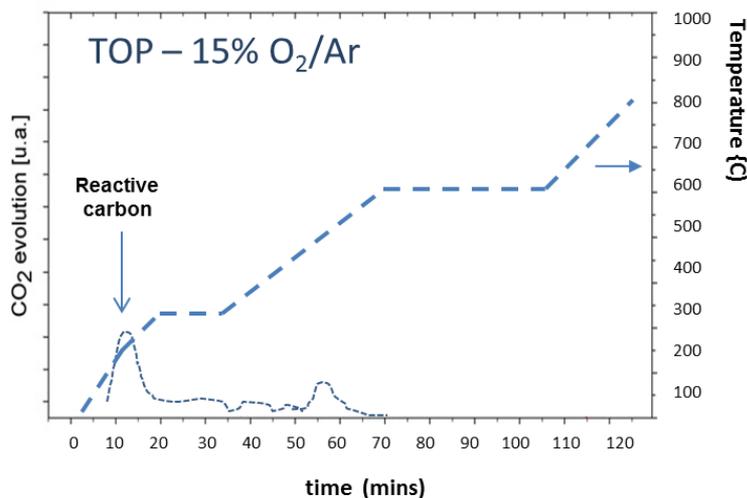


## Spent catalysts analysis

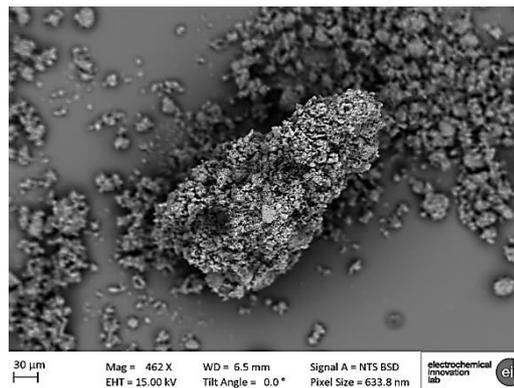
Temperature Programmed Oxidation (TPO) analysis of the catalyst samples from the first methanation reactor clearly showed that during trials almost no polymeric carbon was formed nor detectable sulphur was deposited.



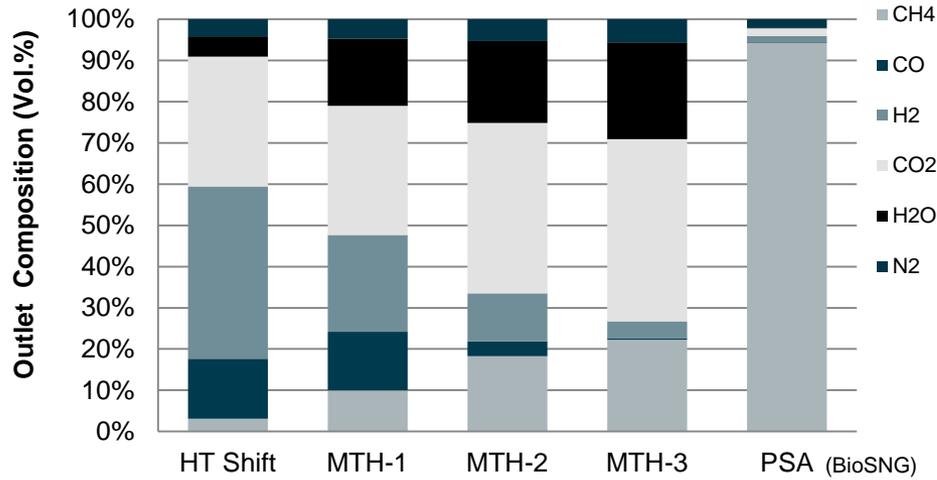
Transmission electron microscopy (TEM) showing Ni particles (black) and surface carbon



SEM image (X470) with Back-scattered electrons (BSE)



# Final BioSNG product



	GS(M)R	Pilot
<b>Sulphur</b>	< 50 mg/m <sup>3</sup>	None
<b>H<sub>2</sub></b>	< 0.1 % (molar)	0.1 – 1.5%
<b>O<sub>2</sub></b>	< 0.2 % (molar)	None
<b>Wobbe</b>	> 47,2 MJ/m <sup>3</sup> < 51,4 MJ/m <sup>3</sup>	35.0-41.6 MJ/m <sup>3</sup> (pre-enrichment)
<b>Other impurities</b>	No liquid below HC dewpoint	None



# FULL CHAIN 4.5 MW<sub>TH</sub> SMALL COMMERCIAL FACILITY

SECURED,  
RESIDUAL WASTE

CONVERSION TO HIGH  
QUALITY SYNGAS

CONVERSION TO  
BioSNG

NETWORK DELIVERY  
& HGV FLEET



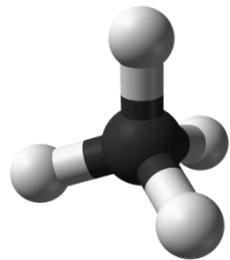
CO<sub>2</sub> SALES



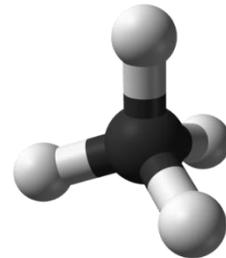
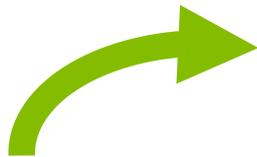
**THE WORLD'S FIRST GRID CONNECTED, FULL CHAIN, WASTE TO SNG FACILITY OPERATING UNDER COMMERCIAL CONDITIONS**

## *Pathways to deeper decarbonization*

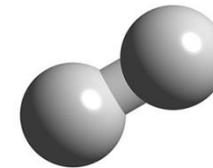
# DEEPER Decarbonisation Route Maps



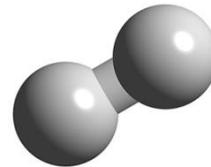
BIOSNG



BIOSNG WITH CCS



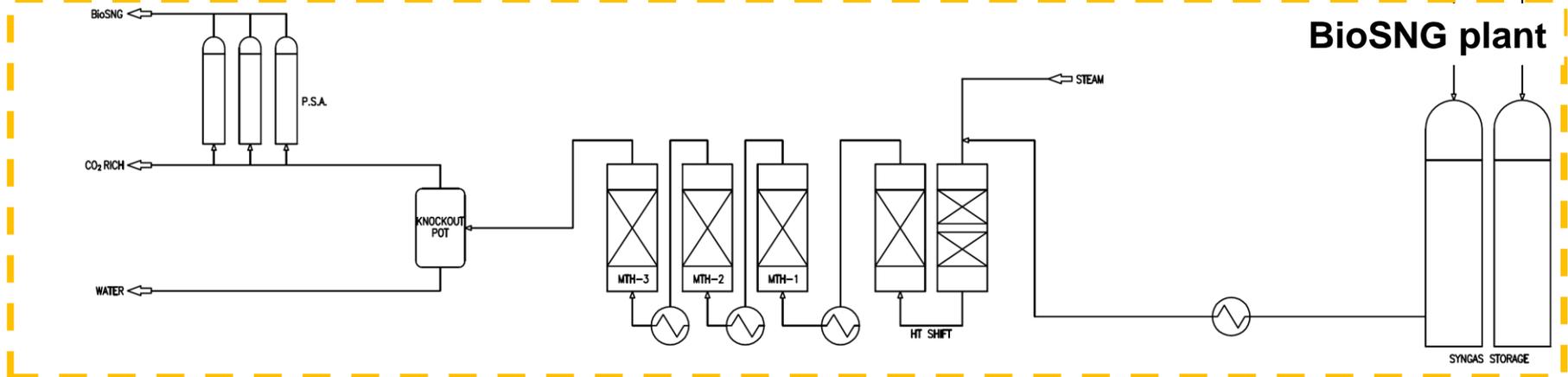
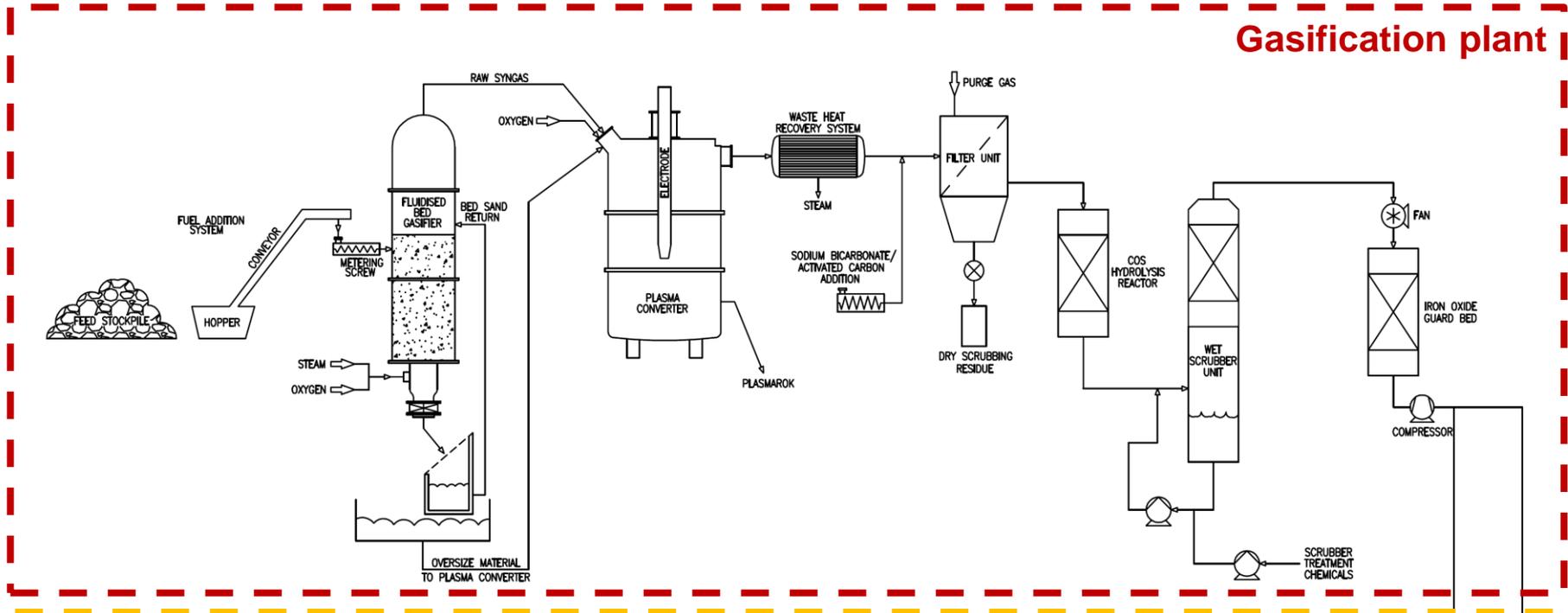
BIOHYDROGEN WITH CCS



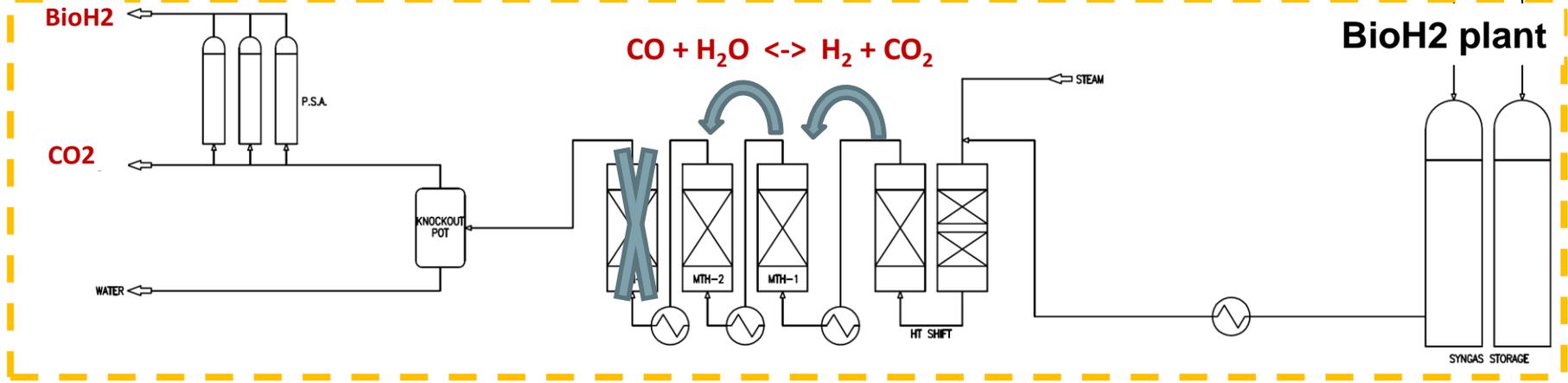
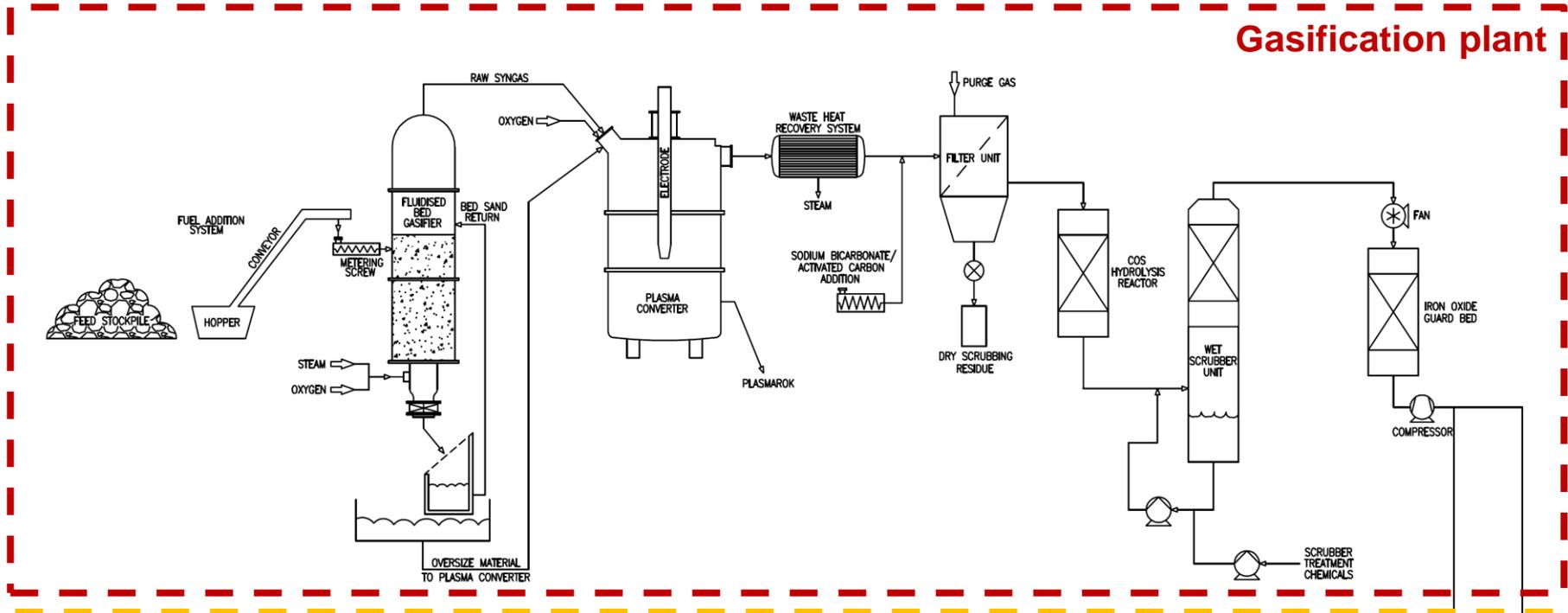
BIOHYDROGEN



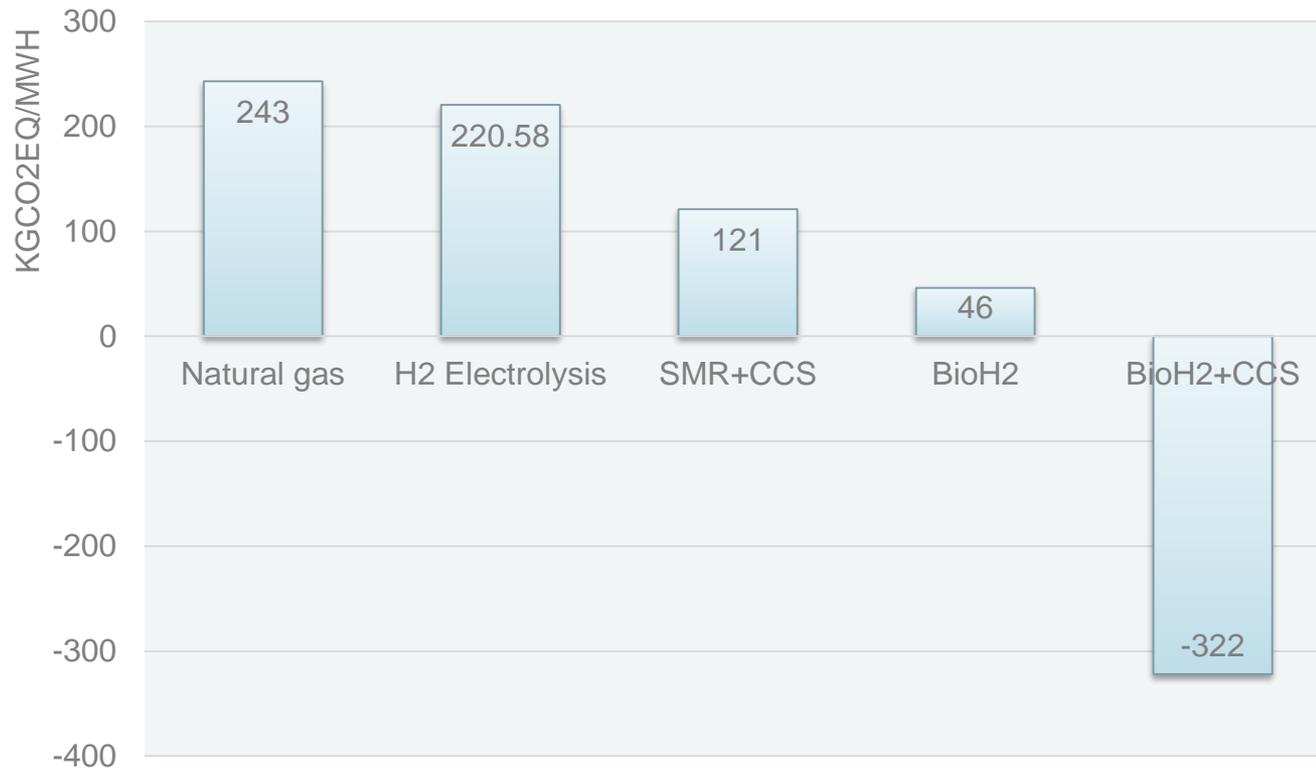
# Pilot plant configuration



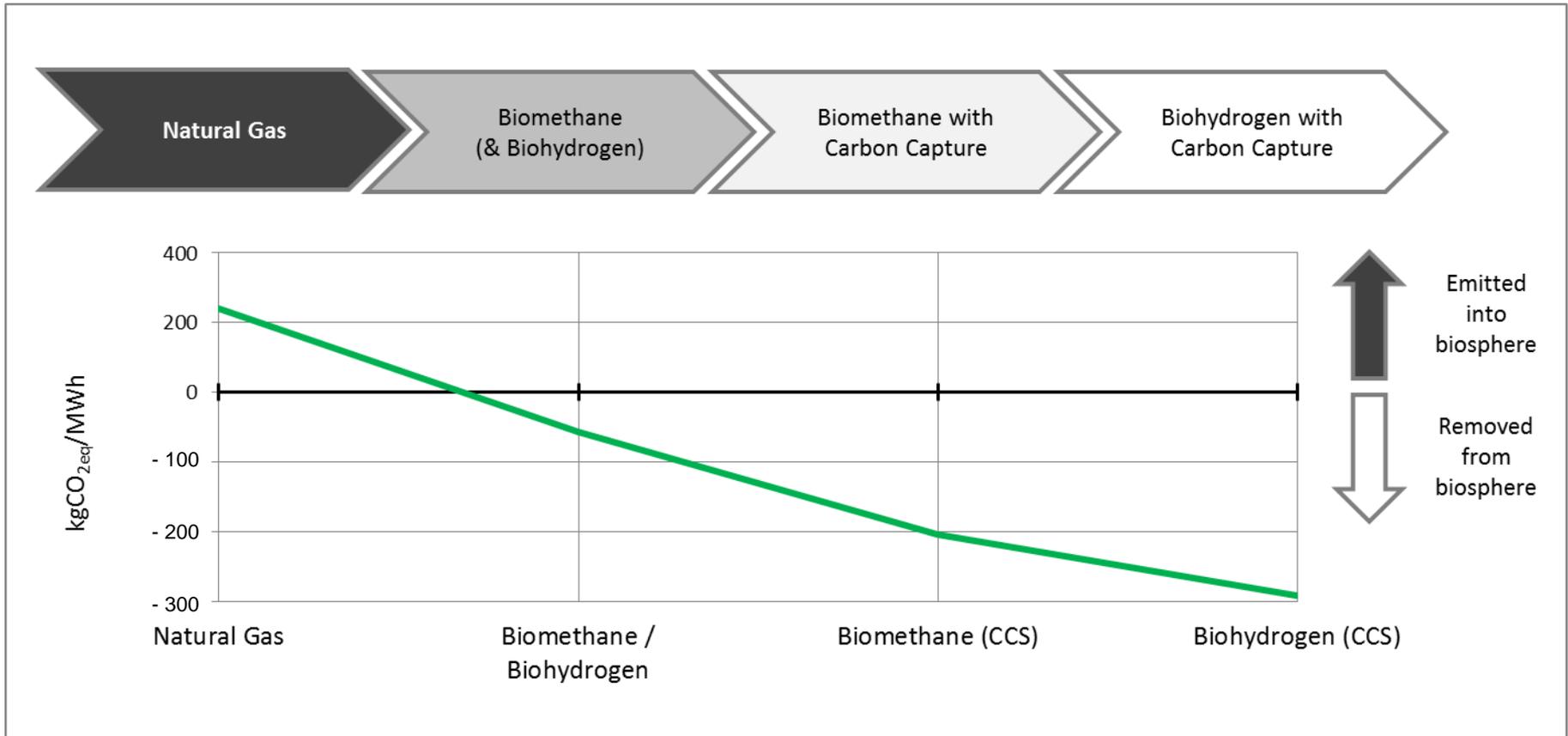
# Pilot plant configuration



# A Pathway to deep carbon savings



# A Pathway to deep carbon savings



# Summary

*GASIFICATION WILL ENABLE THE CONVERSION OF THE UK'S LARGEST SOURCE OF RENEWABLE CARBON TO ALTERNATIVE FUELS TO MEET HEAT & TRANSPORT DEMAND.*



## Challenges:

- The technical approach needs piloting and sustained operation on real waste
- R&D efforts for new technologies to increase availability

# Thank you

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