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# Application of Functional Safety to a Burner Management System – How to Avoid Common Pitfalls

# Bio: Mike Scott

- ▶ B.S. Mechanical Engineering - University of Maryland
- ▶ Masters of Engineering - University of South Carolina
- ▶ Licensed Professional Engineer - AK, GA, SC, and IL
- ▶ Certified Functional Safety Expert (CFSE)
- ▶ IEC 61511 committee member
- ▶ ISA Fellow
  - ▶ Co-Chairman of ISA S84 committee on Electrical/Electronic/Programmable Electronic Systems (E/E/PES) for Use in Process Safety Applications
    - Co-Chairman ISA S84 BMS sub-committee member on Burner Management Systems
    - Past Chairman of the ISA S84 Working Group on Performance Based Fire & Gas Systems
- ▶ Granted 7-US Patents on Safety Lifecycle
- ▶ Embedded Process Safety / Functional Safety role for 18 sites



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- ▶ Burner Management Systems (BMS) are a very common unit operation in the Process Industry
- ▶ However, when LOPA is applied to a BMS it often results in:
  - Incorrect Safety Instrumented Function definition
  - Orders of magnitude differences in Safety Integrity Level (SIL) targets for like unit operations
- ▶ This results in:
  - Increased risk to end user
  - Increased cost of ownership to end user
  - Confusion to Operations and Maintenance on BMS Safety Critical Equipment





- ▶ Inconsistent consequence selection
- ▶ Incorrect SIF definitions
- ▶ Incorrect Cause / Consequence Pairings
- ▶ Too high of SIL targets – e.g., SIL 3
- ▶ High Demand Mode selection
- ▶ Instrumentation Furnished with Packaged Equipment
- ▶ BMS / BPCS combined in a single logic solver as part of an OEM burner upgrade



**Goal: Avoid your name and the words *critical path* being used in the same sentence!**

- ▶ Consistency in Risk Ranking like Fired Equipment across the organization
- ▶ Consistency in SIF definition from site to site for like Fired Equipment
- ▶ Eliminate potential unnecessary spend to modify BMS related SIFs to meet over inflated RRF targets
- ▶ Eliminate potential increased risk associated with missing SIFs or SIL targets that are too low
- ▶ If any risk gaps are uncovered, end user can confidently make decisions on spend / gap closure knowing risk analysis has been approved by corporate SME and is consistent from site to site

The graphic consists of the word 'OUR' in white, bold, sans-serif font inside a green square with a white border. To the right of the square, the word 'OBJECTIVES' is written in a larger, bold, black, sans-serif font.

**OUR OBJECTIVES**

# Develop Fired Device Guidance Notes



► Develop Guidance Notes on typical Fired Equipment in your organization

► Guidance Note to include:

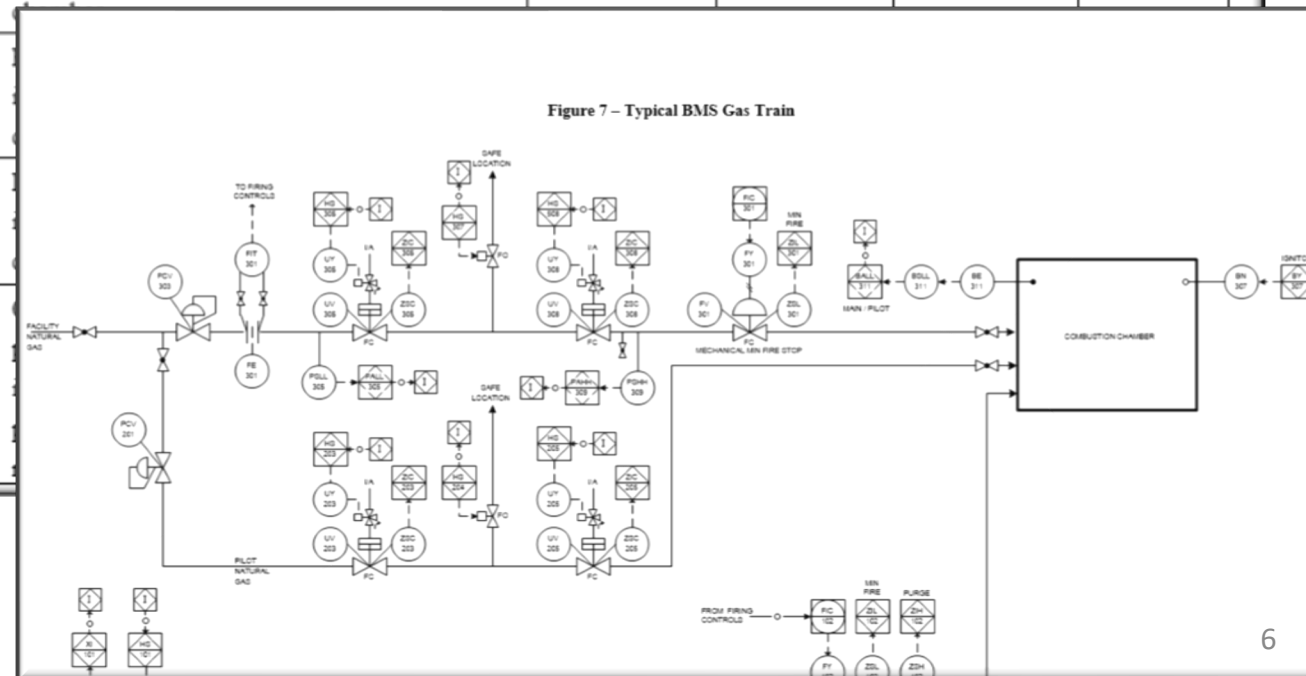
- Consequence Selection
- Independent Protection Layer Guidance
- Typical SIF definitions
- Typical expected SIL targets
- Typical SIS deliverables
- Etc.

Table 1 – Typical BMS Hazards and Associated Safety Instrumented Functions

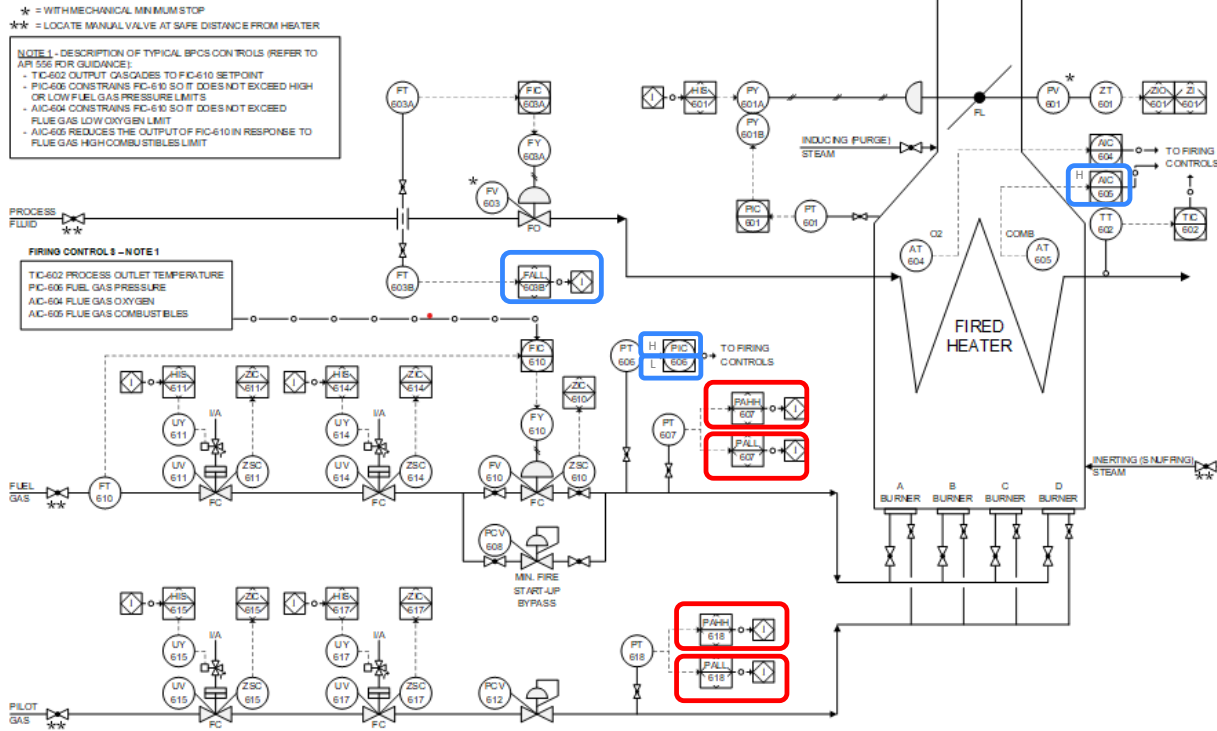
SIF #	Hazard Description	Causes	Sensors	Final Elements	Additional Actions
SIF-001	Low combustion air flow causes unstable flame operation and loss of flame	<ul style="list-style-type: none"> <li>• Combustion Air Fan failure</li> <li>• Combustion air</li> </ul>	PSLL-103 or BSLL-311	Close UV-306 or UV-308	<ul style="list-style-type: none"> <li>• Open main vent valve (UV-307)</li> <li>• Maintain combustion air</li> </ul>

Table 2 – Typical BMS Safety Integrity Level Calculations

SIF #	SIF Description	Target SIL PFDavg – Note 1	Test Interval	SIL Arch Constraints	Achieved SIL – Note 1
SIF-001	Low low combustion air flow or loss of flame isolates main burner fuel gas to combustion	2	12 Months	2	2



# Document Centric Approach Multi-Burner Heater



NOTE 1 - DESCRIPTION OF TYPICAL BPCS CONTROLS (REFER TO APR 556 FOR GUIDANCE):

- TIC-602 OUTPUT GAS/GASES TO FIC-610 SETPOINT
- PIC-605 CONSTRAINS FIC-610 SO IT DOES NOT EXCEED HIGH OR LOW FUEL GAS PRESSURE LIMITS
- AIC-604 CONSTRAINS FIC-610 SO IT DOES NOT EXCEED FLUE GAS LOW OXYGEN LIMIT
- AIC-605 REDUCES THE OUTPUT OF FIC-610 IN RESPONSE TO FLUE GAS HIGH COMBUSTIBLES LIMIT

FIRING CONTROLS - NOTE 1

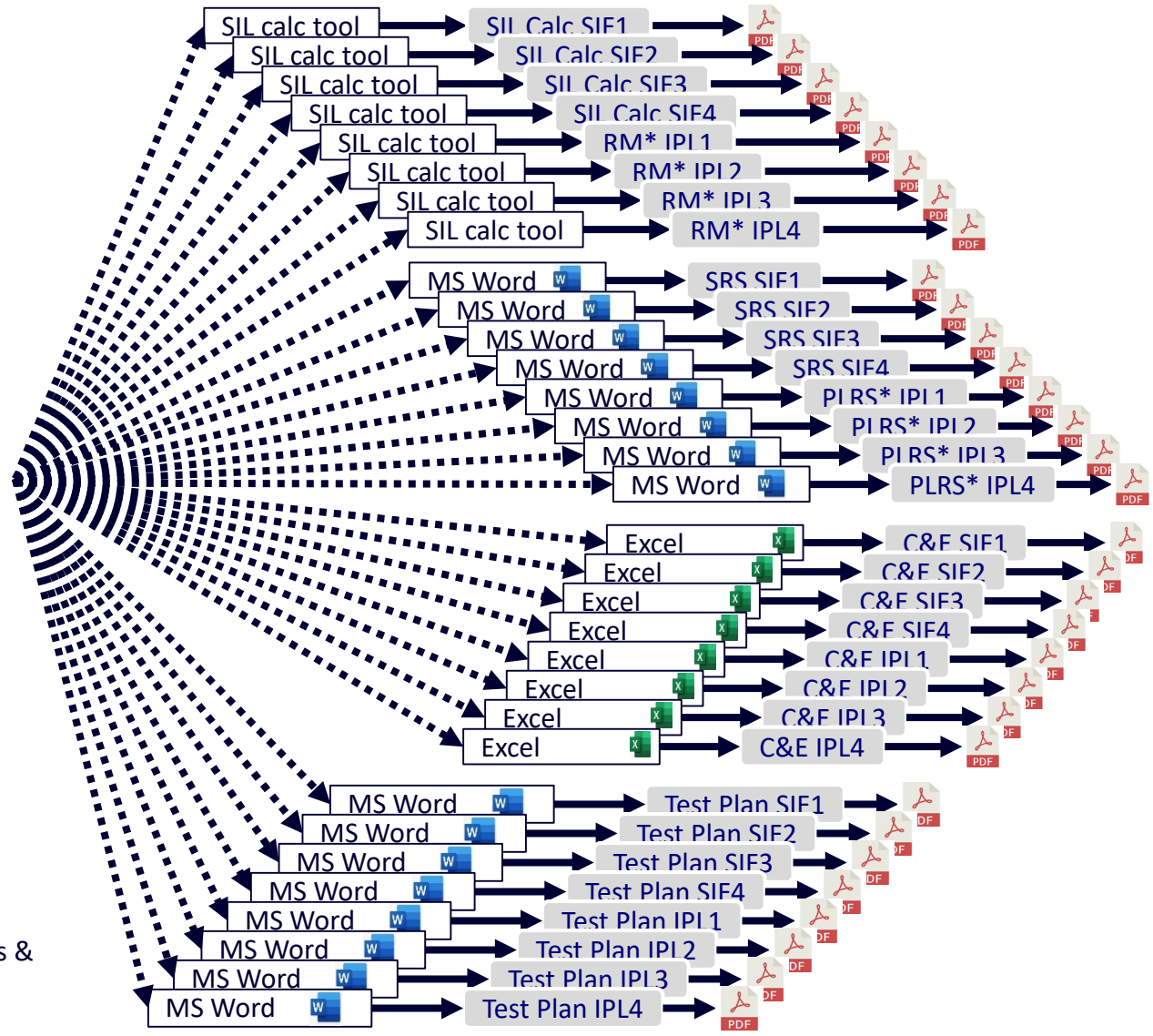
- TIC-602 PROCESS OUTLET TEMPERATURE
- PIC-606 FUEL GAS PRESSURE
- AIC-604 FLUE GAS OXYGEN
- AIC-605 FLUE GAS COMBUSTIBLES

**SIF**

**IPL**

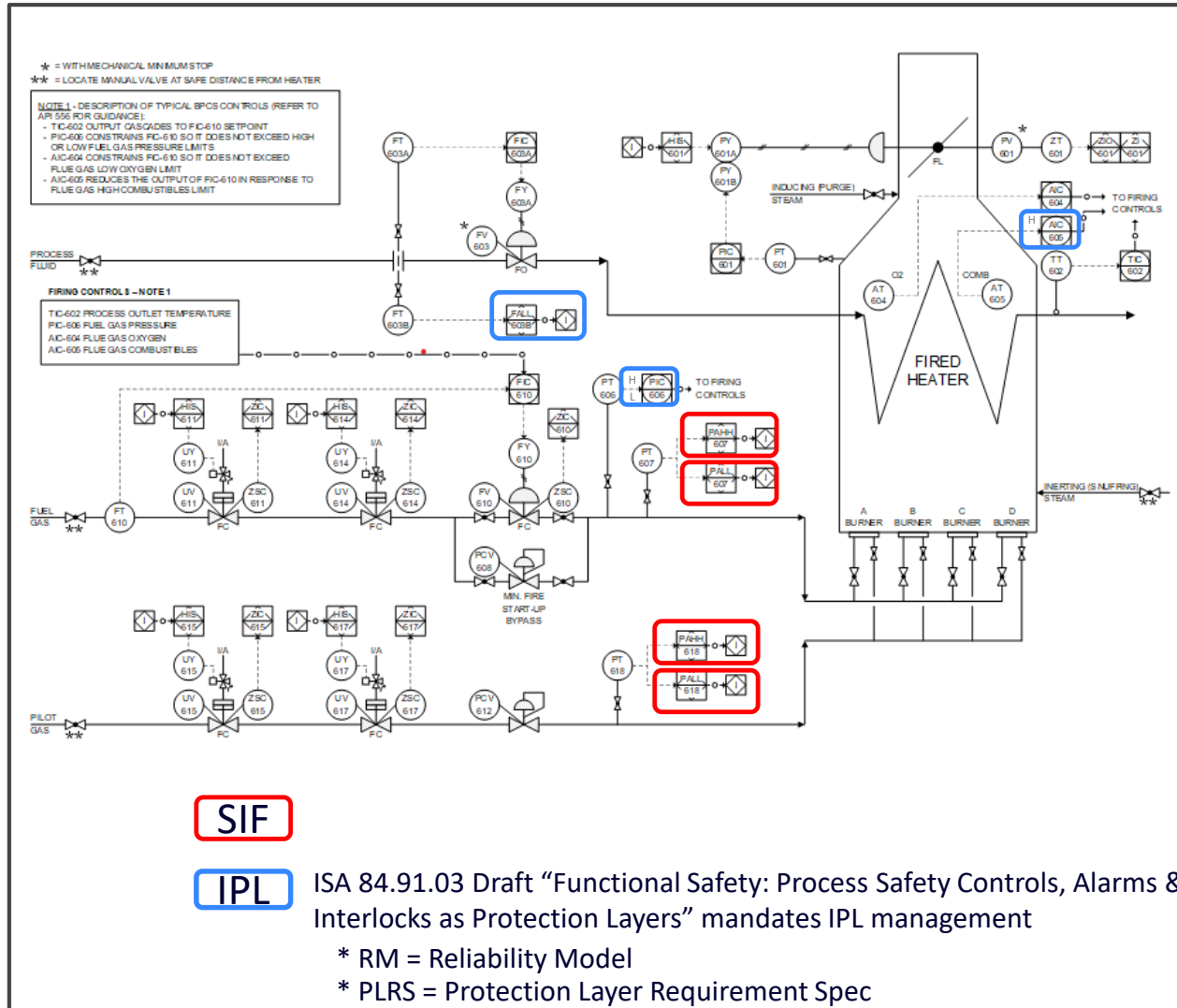
ISA 84.91.03 Draft "Functional Safety: Process Safety Controls, Alarms & Interlocks as Protection Layers" mandates IPL management

- \* RM = Reliability Model
- \* PLRS = Protection Layer Requirement Spec



**Manually Enter Data For Each SIF/IPL To Comply with IEC 61511**

# Templatization Approach Multi-Burner Heater



Bulk Insert  
 All Tags  
 &  
 Voting  
 from  
 I/O List

Bulk Update  
 SIL Calcs  
 and  
 Docs for  
 All SIFs  
 & IPLs

8 SIL Calcs/RMs

8 SRS/PLRS

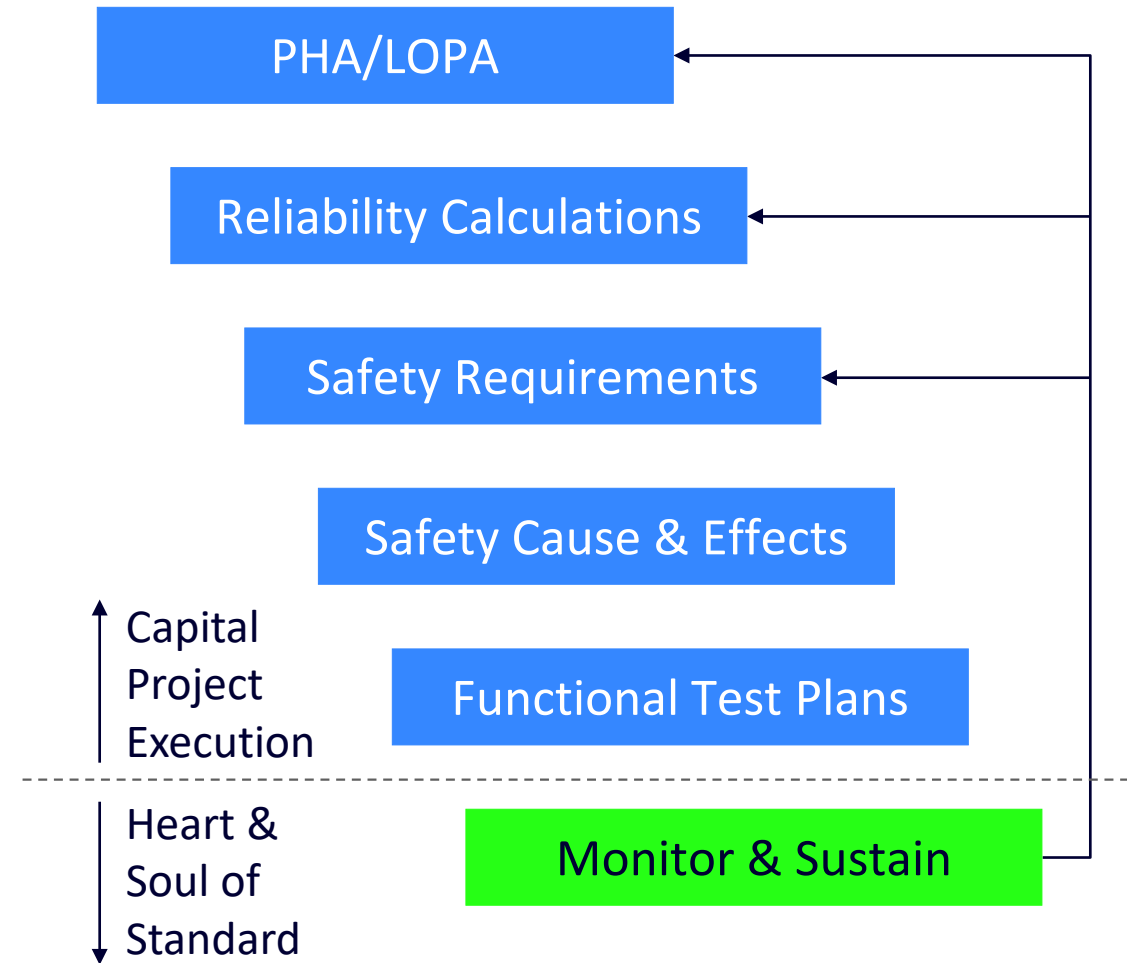
8 C&E

8 Test Plans

Reduced Time to Complete IEC 61511 Docs from >40 hours to <1 Hour



# End Goal of IEC 61511



Single Connected Data Model  
to Drive Fired Heater KPIs



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Questions?