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# Validation of CFD models to predict hydrodynamics of stirred tank flows in the transitional flow regime.

Georgina Wadsley<sup>1,2</sup>

David F. Fletcher<sup>3</sup>

Joelle Aubin<sup>2</sup>

Andy Ingram<sup>1</sup>

Waldo Rosales<sup>4</sup>

Mark J. Simmons<sup>1</sup>

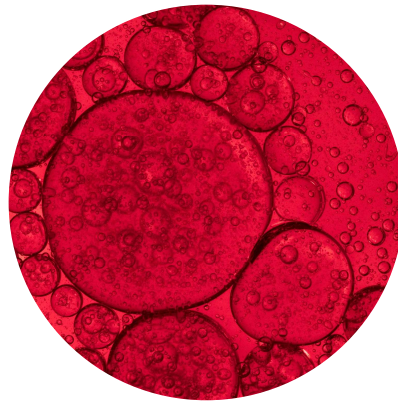
IChemE Fluid Mixing Processes Meeting  
10<sup>th</sup> January 2024

<sup>1</sup>School of Chemical Engineering, University of Birmingham, <sup>2</sup>Laboratoire de Génie Chimique, UMR CNRS 5503, <sup>3</sup>School of Chemical and Biomolecular Engineering, University of Sydney, <sup>4</sup>Unilever R&D, Port Sunlight Laboratory

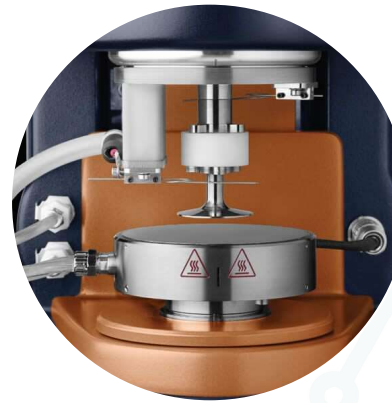
# Project Context



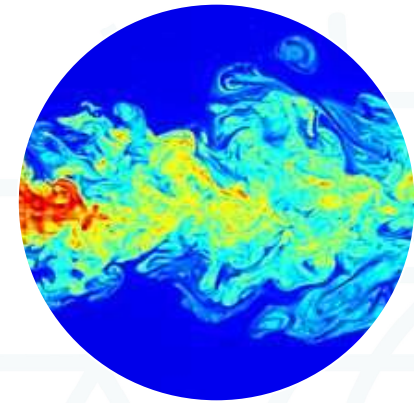
Home & personal care products



Multiphase formulations

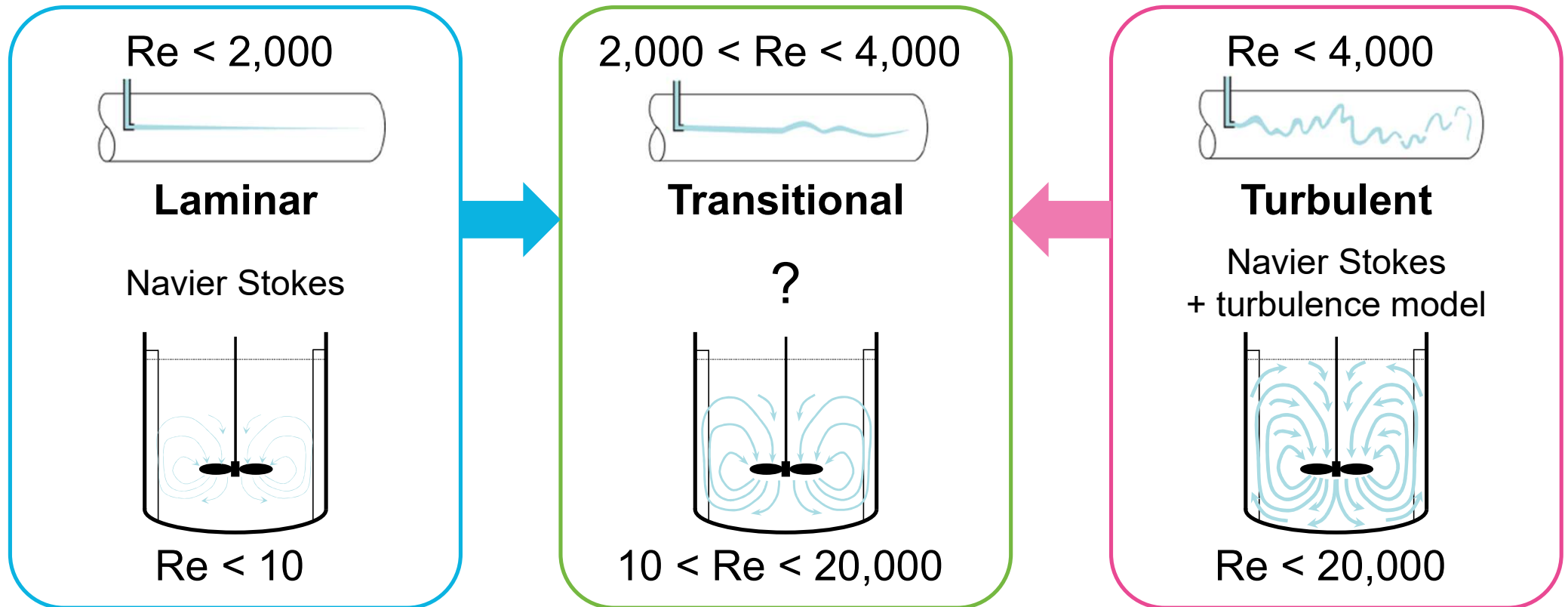


Complex rheology & microstructure



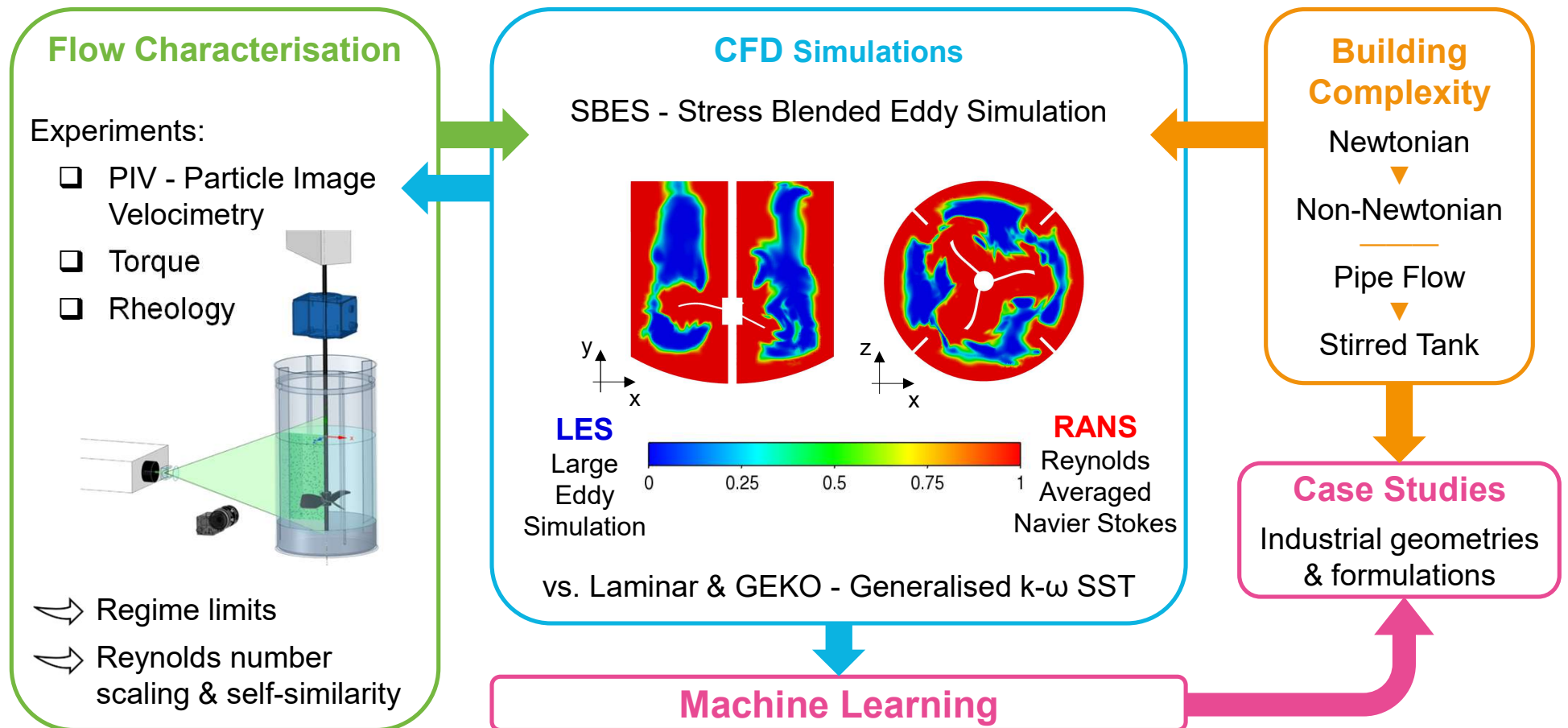
Transition between flow regimes

# State of the Art - Modelling of Transitional Flows



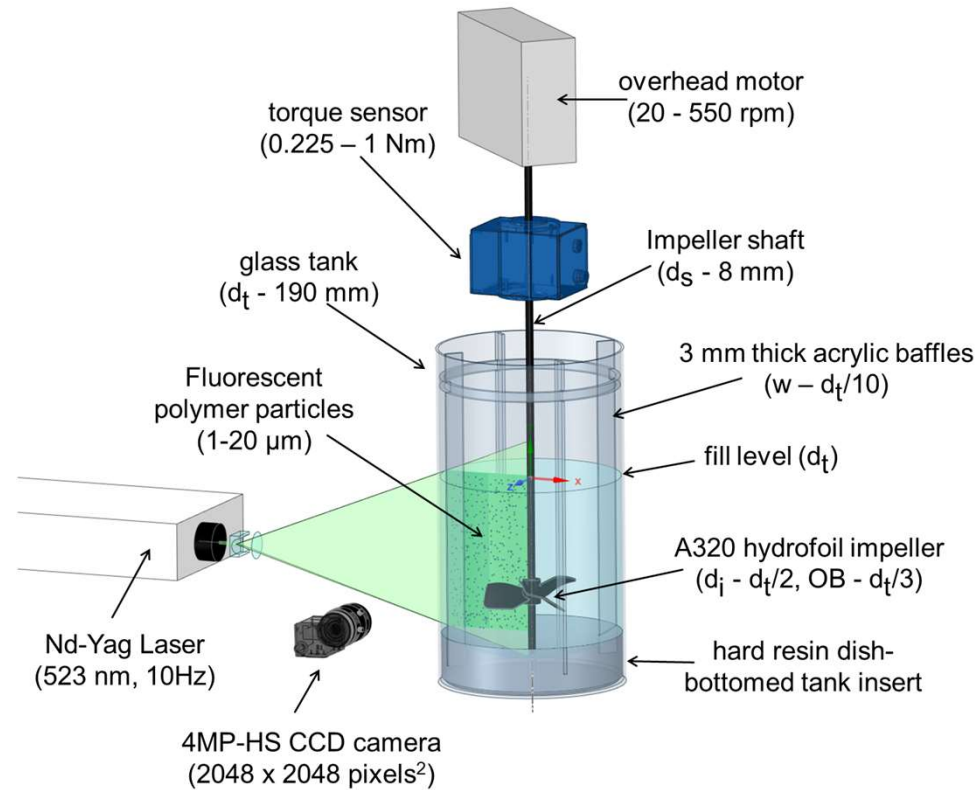
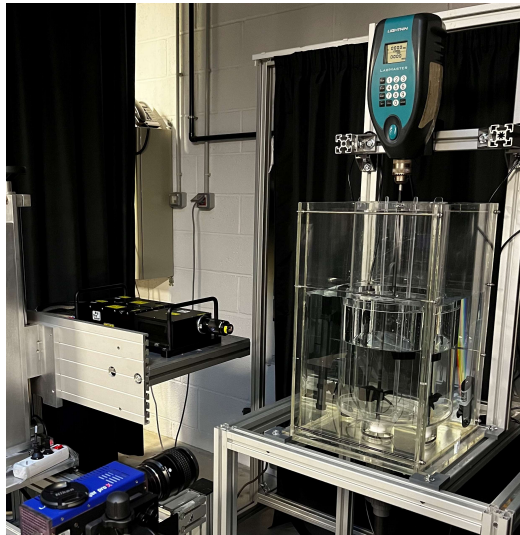
# Aims - Investigative Approach

“Prediction of complex industrial flows in the transitional regime”

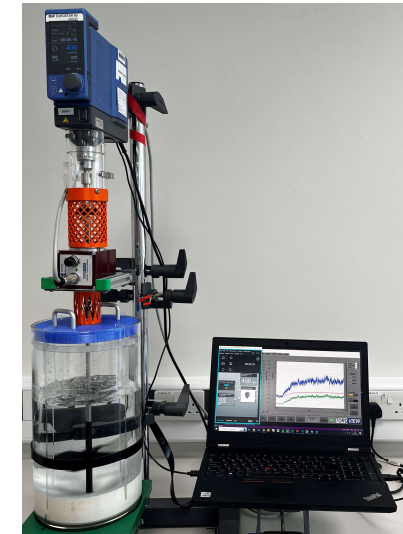


# Experimental Set-Up

**PIV 5 L**



**Torque 5 L**

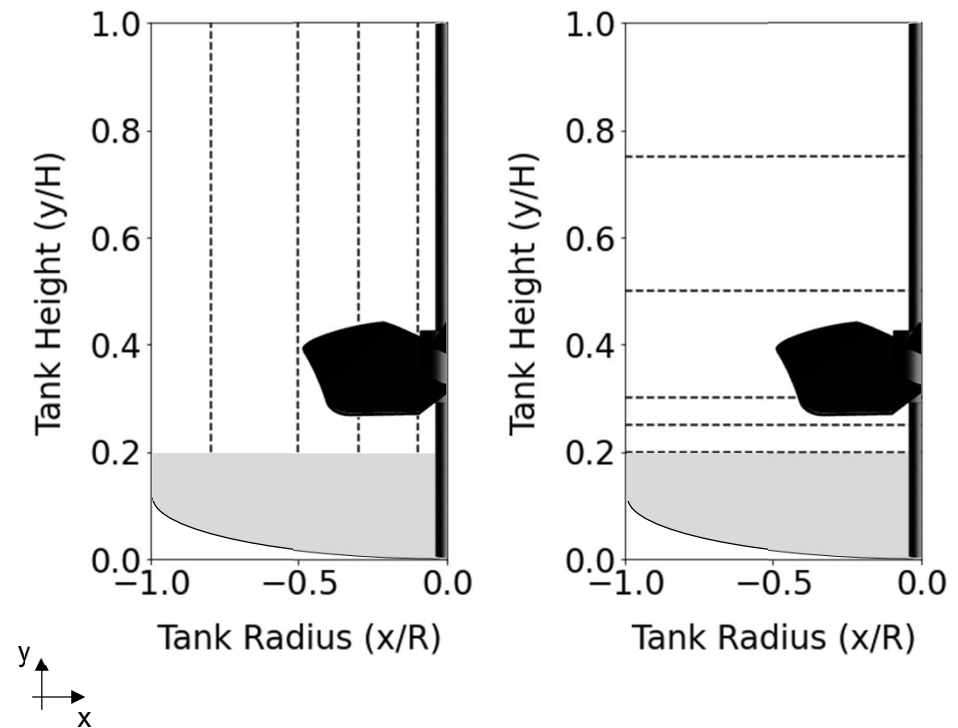


**Torque 170 L**

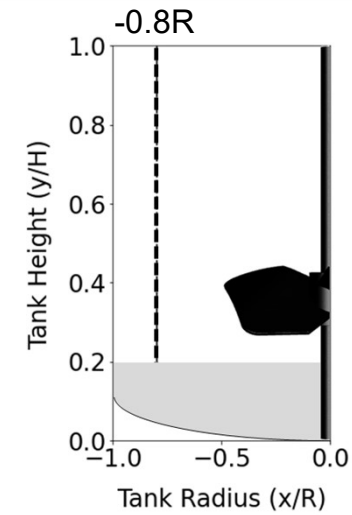
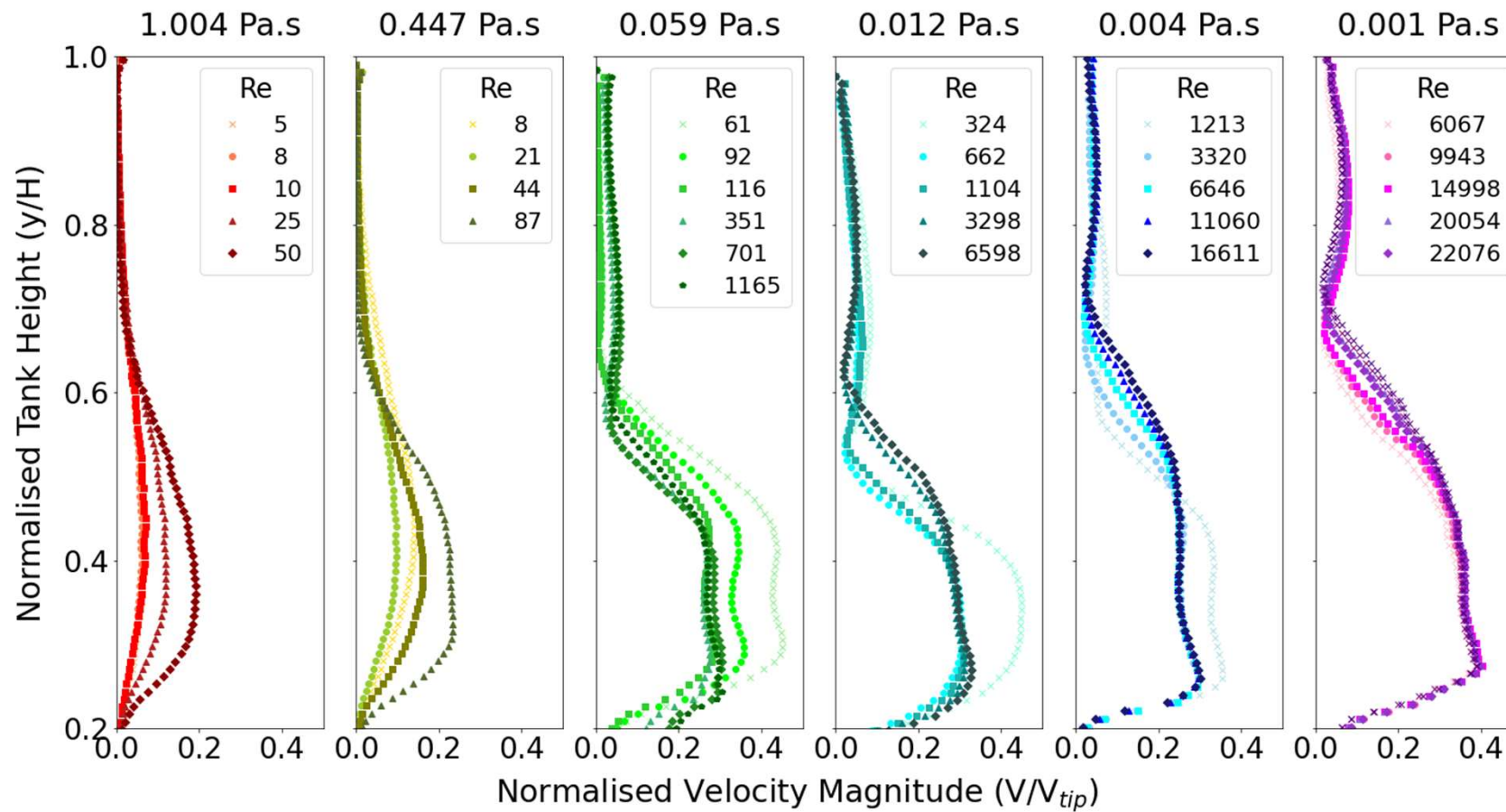


# Stirred Tank Investigation – PIV & Torque

- ❑ **Re** = 5 – 35,000
  - ❑ **V<sub>tip</sub>** 0.1 – 2.7 m/s
  - ❑ **μ** (apparent) 1.5 – 0.001 Pa.s
    - ❑ Glycerol (40 – 100 wt%)
    - ❑ CMC (0.1 – 0.2 wt%)
- ❑ Observe trends of normalised velocity magnitude & fluctuations
  - ❑  $\Delta$  Re, constant  $\mu$
  - ❑  $\Delta$   $\mu$ , constant Re
  - ❑ Newtonian vs non-Newtonian



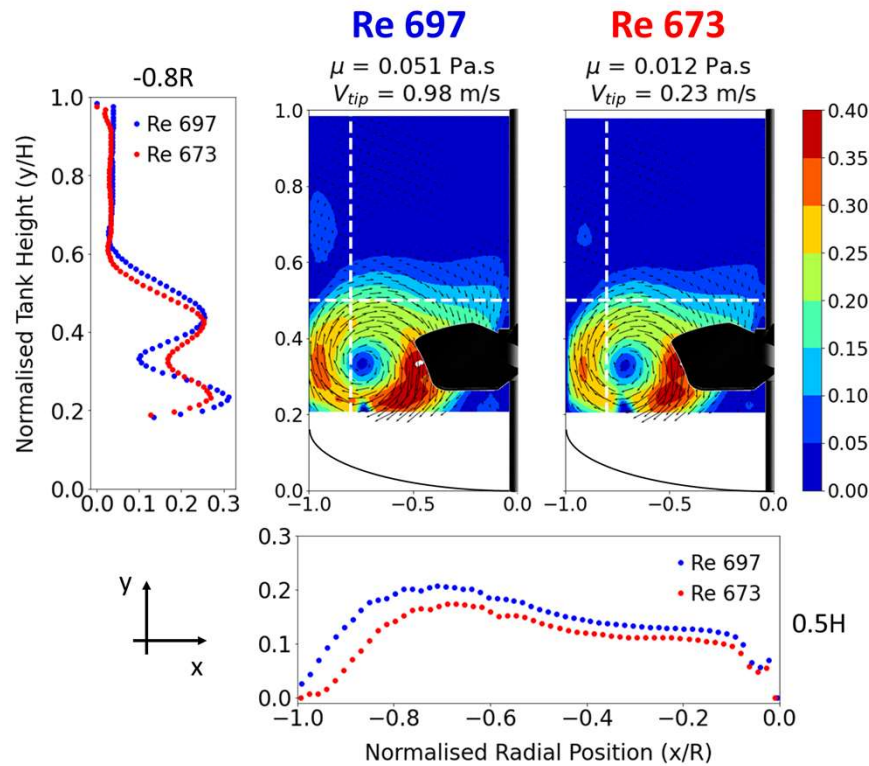
# PIV Results - $\Delta$ Re, constant $\mu$



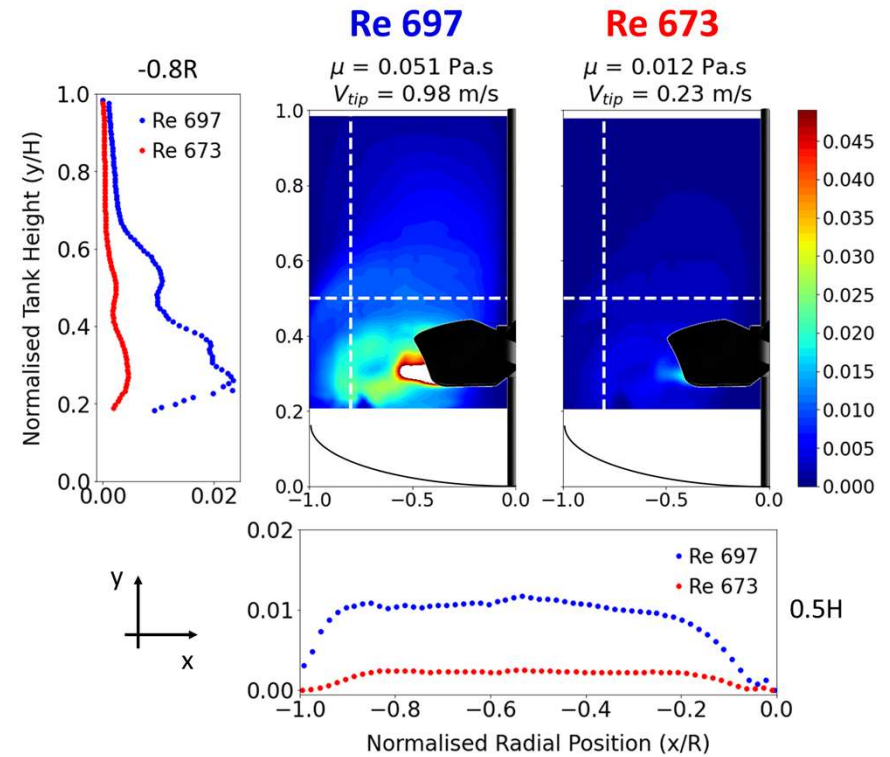
# PIV Results - $\Delta \mu$ , constant Re

$$V_{fluc} = 3/4 \sqrt{\tilde{u}^2 + \tilde{v}^2}$$

Normalised Velocity Magnitude ( $V/V_{tip}$ )

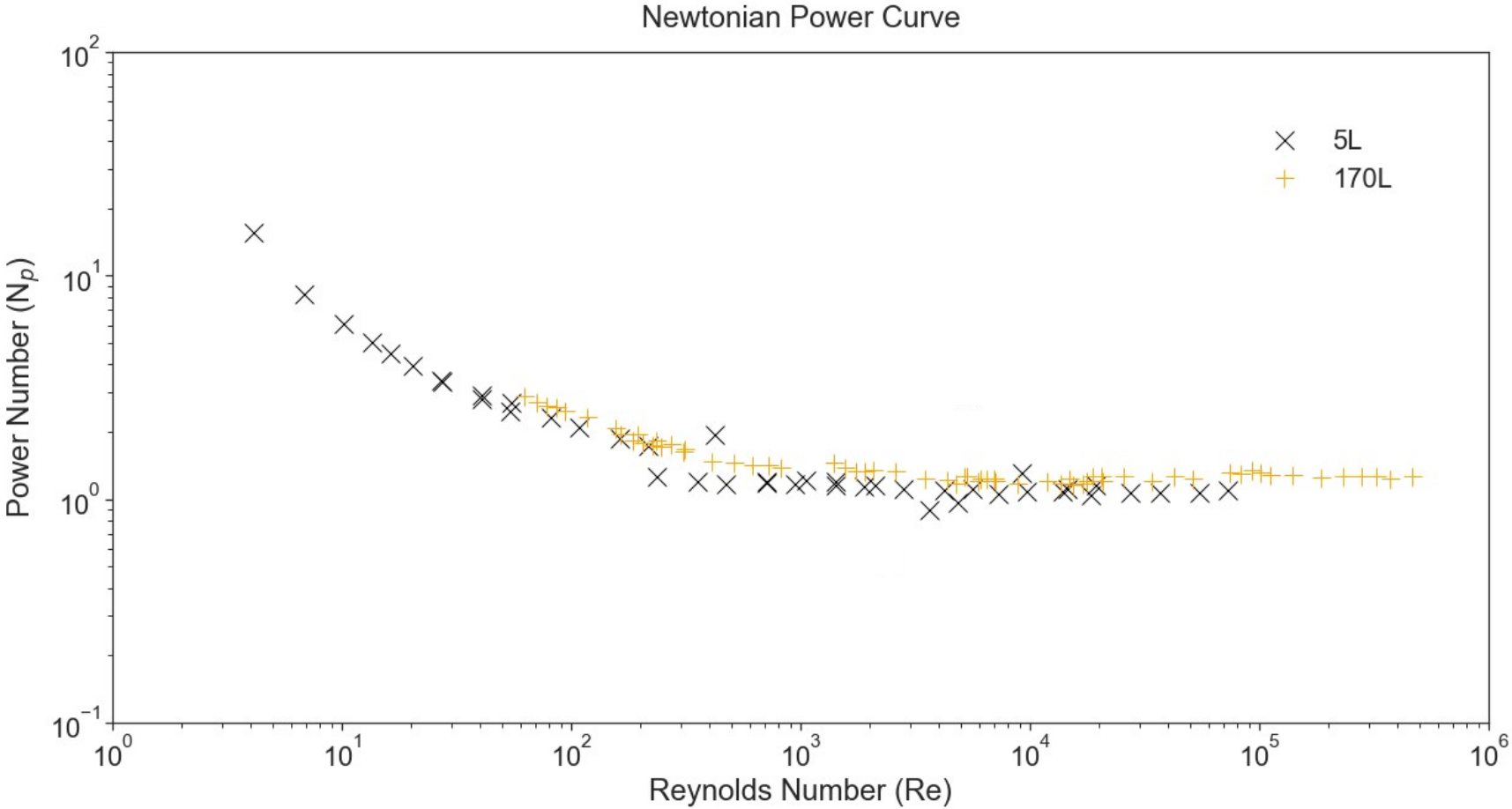


Normalised Velocity Fluctuations ( $V_{fluc}/V_{tip}^2$ )

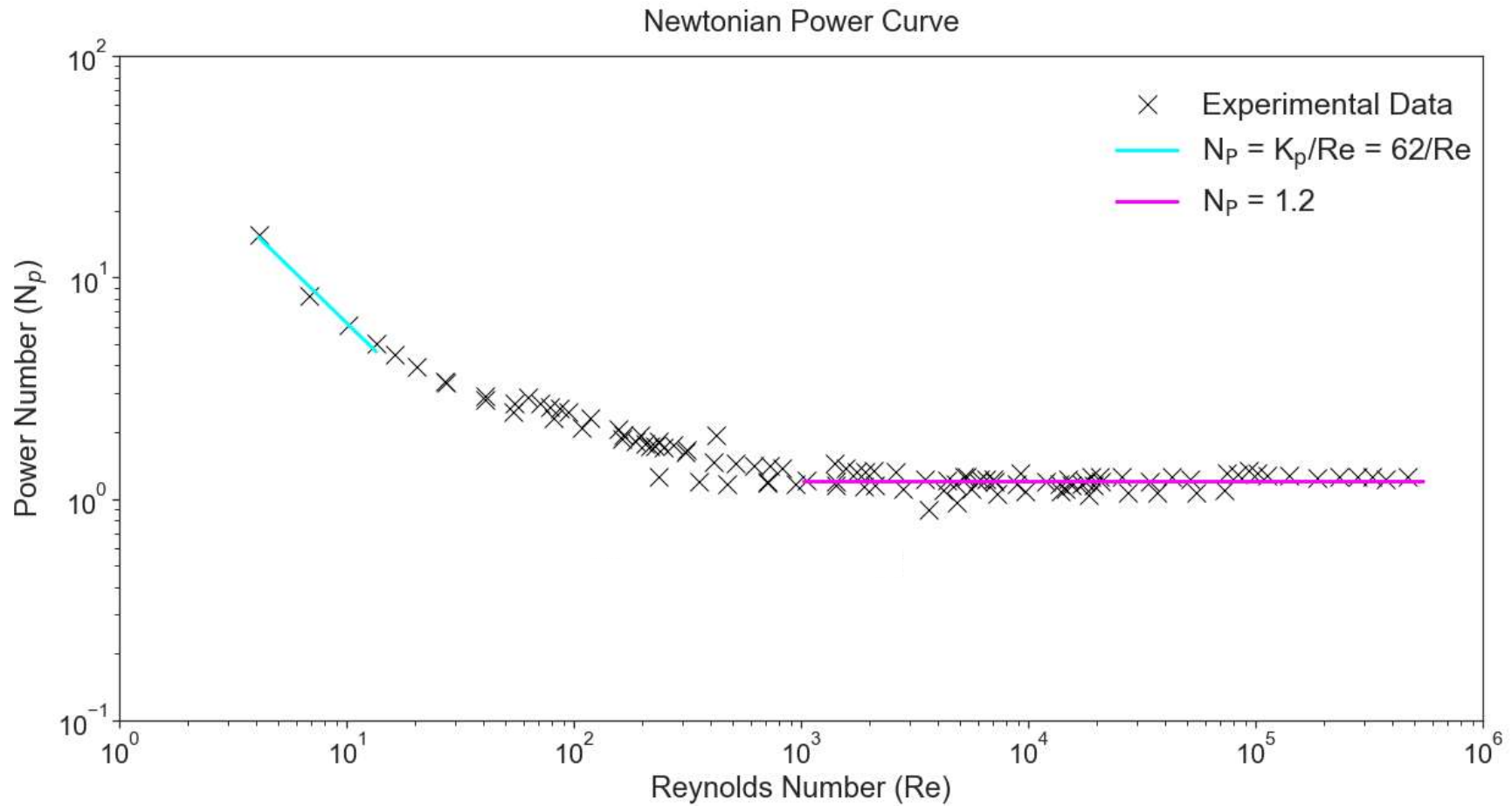




# Torque Results – 5L vs 170 L



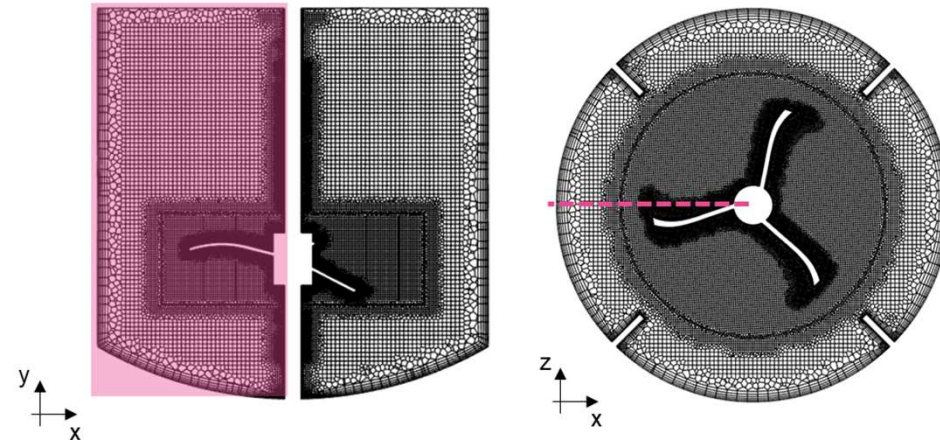
# Torque Results – Laminar & Turbulent Regime Fitting



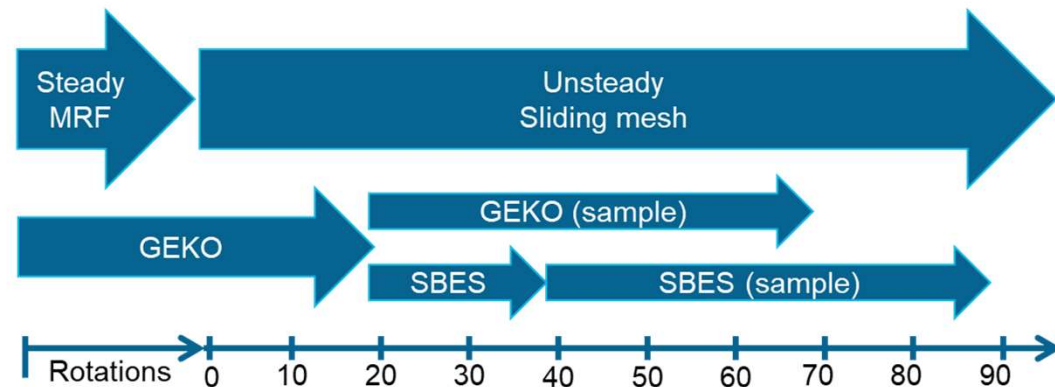
# Simulation Set-up

- ❑ Convergence monitors
  - ❑ Residual values  $< 10^{-6}$
  - ❑ Torque (impeller & walls)
  - ❑ Mass integral of  $\varepsilon$
- ❑ Data sampling on a **fixed plane**
  - ❑ All blade positions
  - ❑ Periodic (every full rotation) - estimate pseudo turbulence due to blade contributions.

## Polyhexcore mesh - 2.14M cells



## Numerical Methods



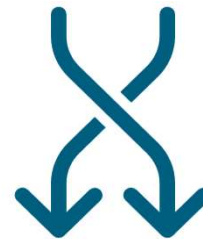
# Scale Resolving Simulations – Why SBES?

## LES

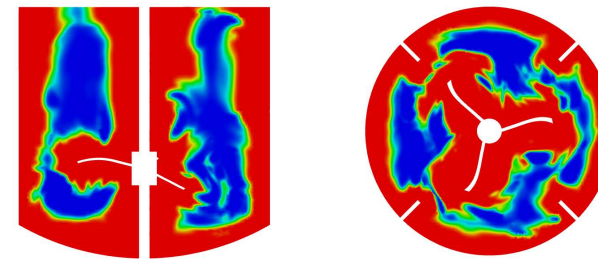
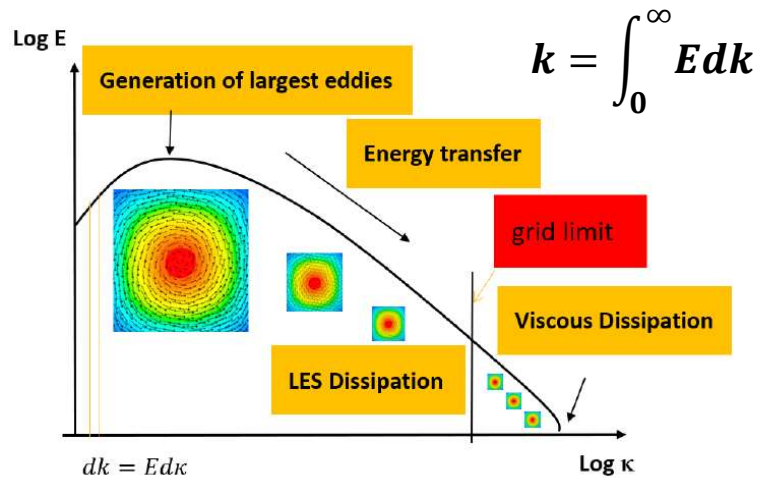
- ❑ spatial filtering of NS
- ❑ resolves large scale turbulence
- ❑ models small scale structures

## RANS

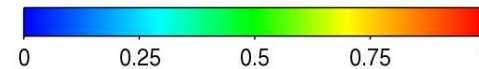
- ❑ averaging of NS
- ❑ must model Reynolds stresses
- ❑ GEKO (k- $\omega$  SST closure model)



SBES



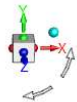
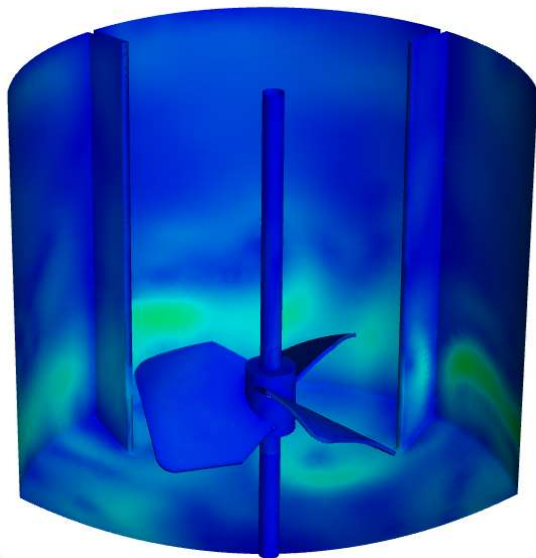
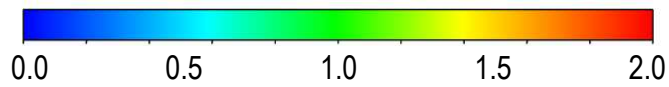
**LES**  
Large  
Eddy  
Simulation



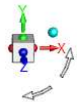
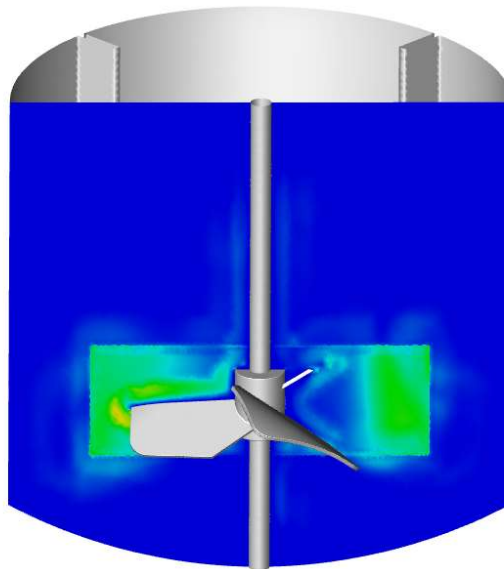
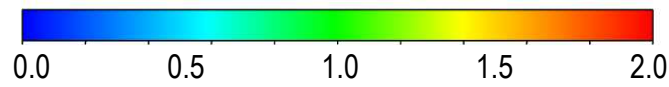
**RANS**  
Reynolds  
Averaged  
Navier Stokes

# Simulation Solution Checks

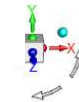
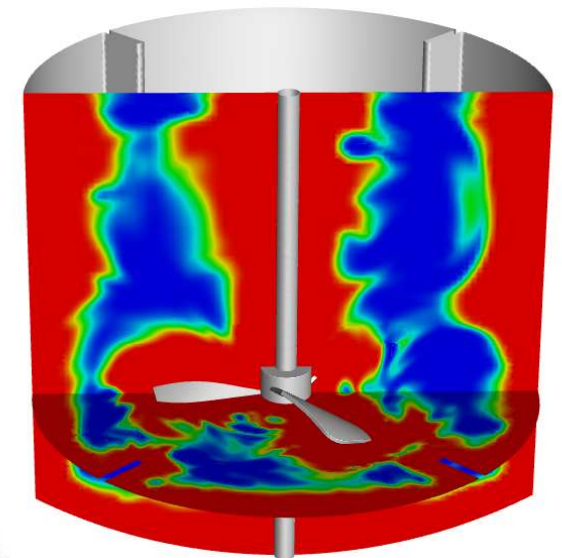
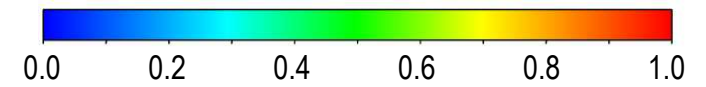
Wall Y+



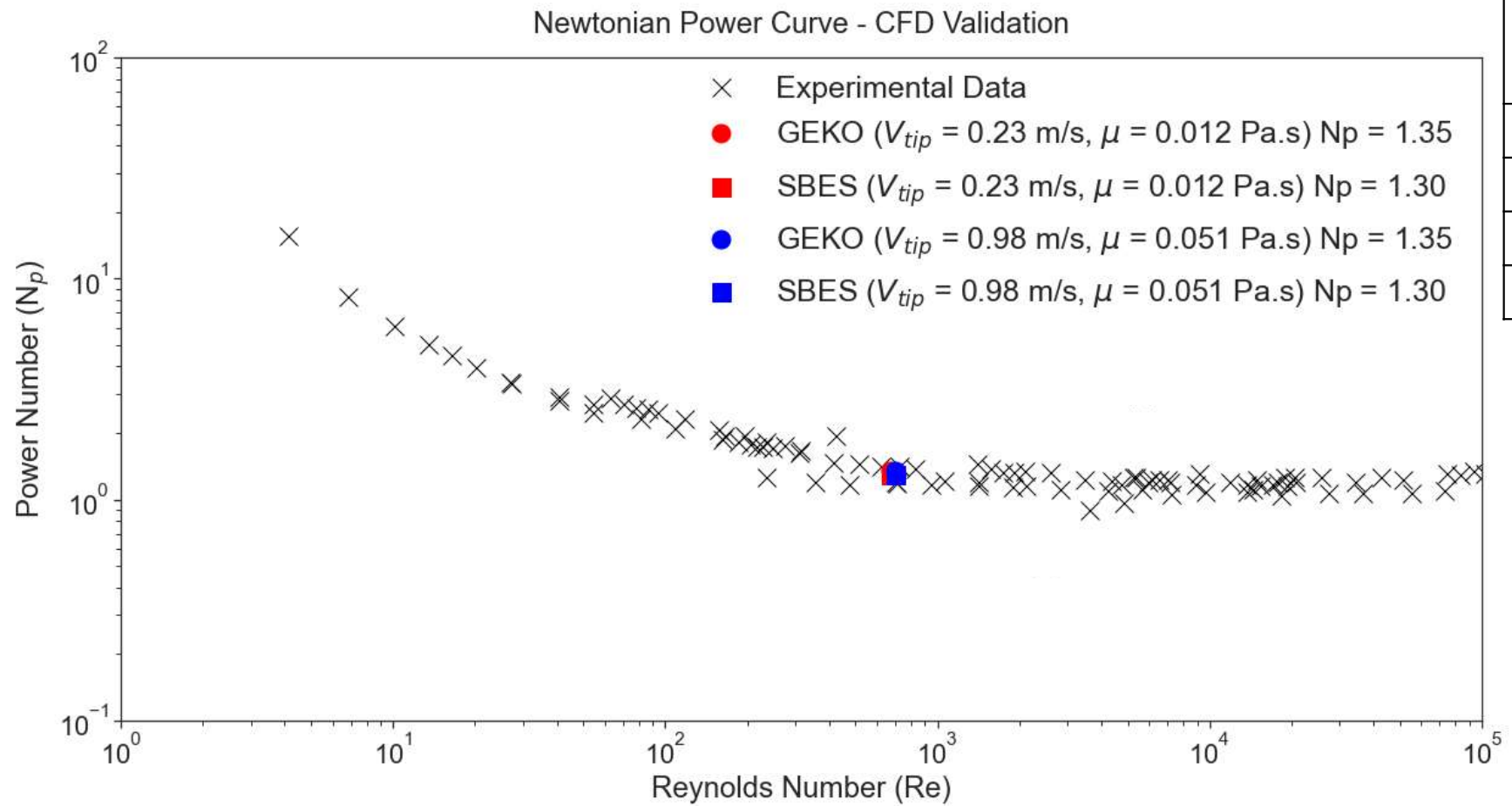
Cell Convective Courant



Blending function for SBES  
(LES = 0, RANS = 1)

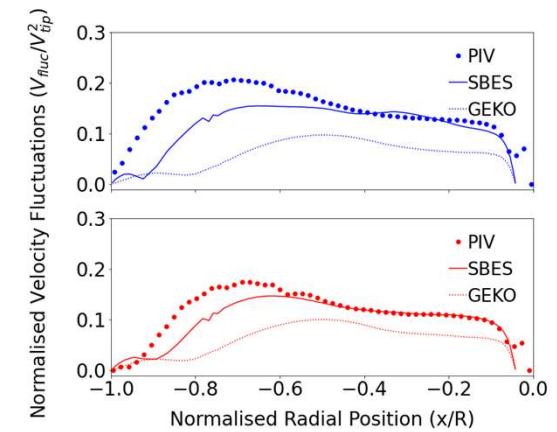
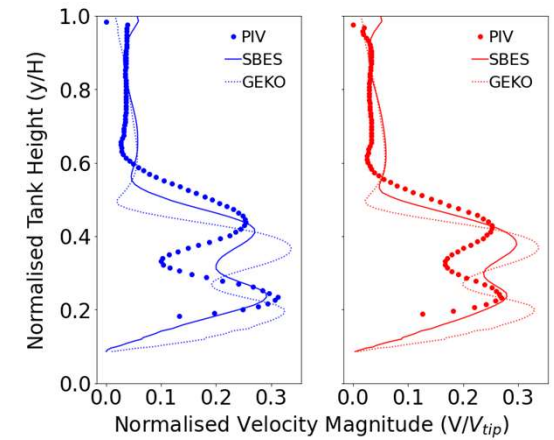
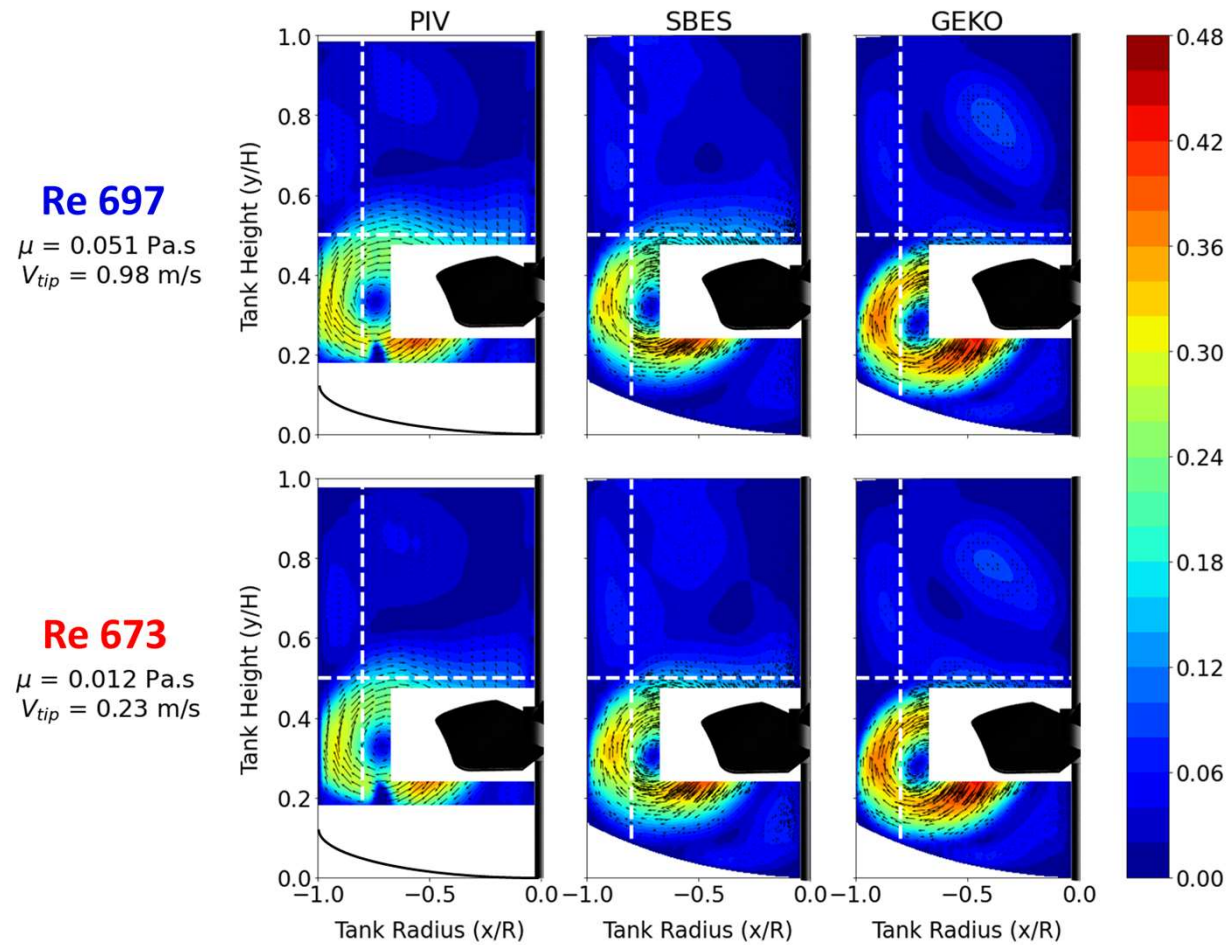


# CFD Validation - Torque



<b><math>N_p</math> from wall torque</b>
1.07
1.33
1.07
1.30

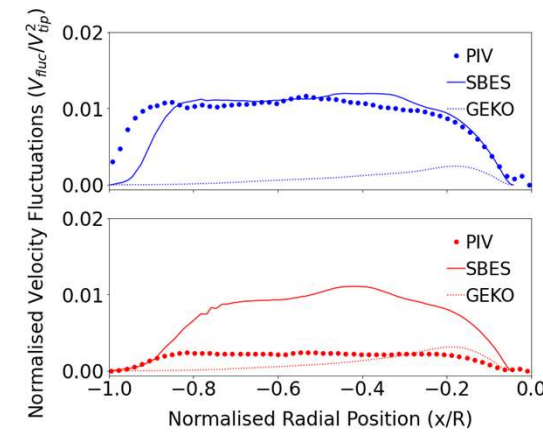
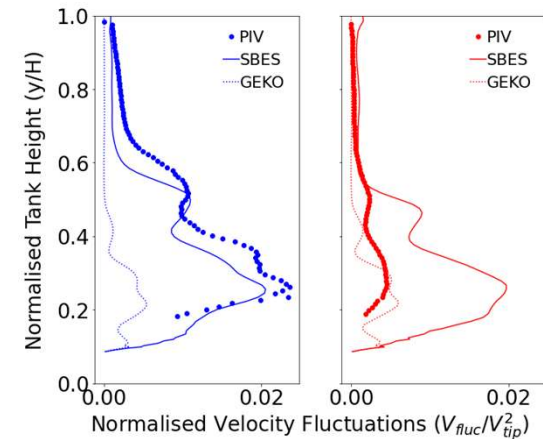
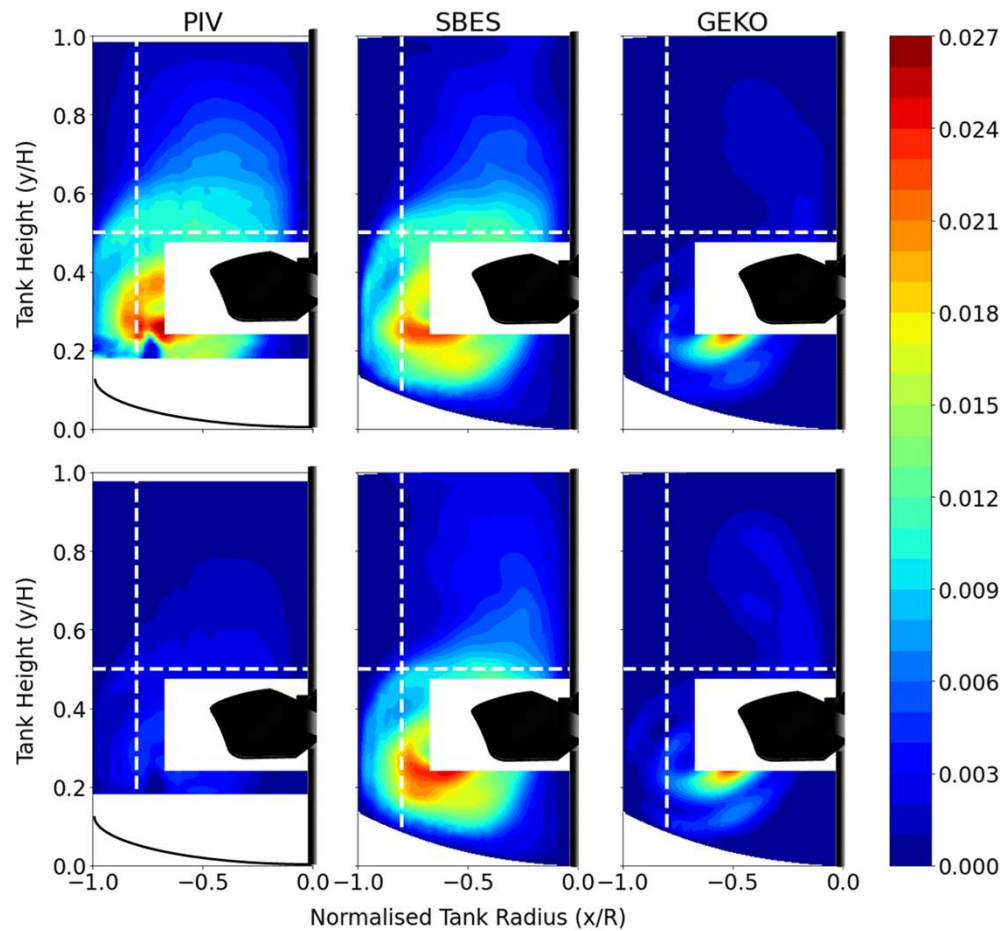
# CFD Validation – Normalised Velocity Magnitude ( $v/v_{tip}$ )



# CFD Validation – Normalised Velocity Fluctuations ( $V_{fluc}/V_{tip}^2$ )

**Re 697**  
 $\mu = 0.051 \text{ Pa}\cdot\text{s}$   
 $V_{tip} = 0.98 \text{ m/s}$

**Re 673**  
 $\mu = 0.012 \text{ Pa}\cdot\text{s}$   
 $V_{tip} = 0.23 \text{ m/s}$





## Conclusions

- ❑ Distinct flow behaviours identified for each flow regime.
- ❑ Transitional regime limits are not constant - vary with fluid viscosity ( $\mu$ ).
- ❑ Transitional regime flows scaled for same Re do not exhibit self-similar flow hydrodynamics.
- ❑ Both GEKO & SBES closure models validated for torque prediction.
- ❑ SBES performs better to predict torque balance & velocity magnitudes.
- ❑ Failure to predict difference in velocity fluctuations between two transitional regime cases with same Re.

## Future Work

- ❑ Fix SBES blending function to run larger region of LES.
- ❑ Confirm both GEKO & SBES accurately predict high Re cases.
- ❑ Explore impeller blade and baffle periodicity using POD & periodic averaging.

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# Thank you

For more information, please get in touch...

Georgina Wadsley

gkw059@student.bham.ac.uk

*Authors acknowledge financial support from the EPSRC Centre for Doctoral Training in Formulation Engineering (EP/S023070/1) and Unilever*

✉ [cdt-formulation@contacts.bham.ac.uk](mailto:cdt-formulation@contacts.bham.ac.uk)      @FormulationCDT

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