

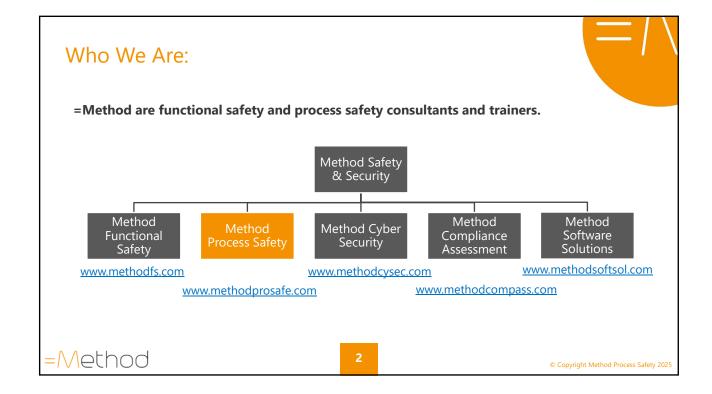
# What Process Engineers Should Know About Functional Safety

# IChemE Irish Members Group & Engineers Ireland, August 2025

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1

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#### What is Process Safety?

#### Safety:

o "Freedom from risk which is not tolerable" – IEC61511

#### Process Safety (CCPS definition):

- Process safety deals with the prevention and control of incidents that have the potential to release hazardous materials or energy.
- Such incidents can cause toxic effects, fire or explosion and could ultimately result in serious injuries, property damage, lost production and environmental impact.





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3

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### What is Functional Safety?

"Part of the overall safety relating to the process & the BPCS which depends on the correct functioning of the SIS & other protection layers" - IEC61511

So functional safety is a key thing we do in order to achieve overall process safety, i.e. freedom from intolerable risk.



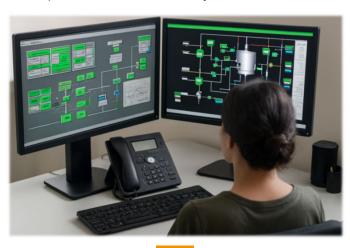
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#### Basic Process Control System (BPCS)

- o The main purpose of the BPCS is to provide continuous control of the process.
- o The BPCS is the main plant DCS or PLC/SCADA system.



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5

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# The Functional Safety Standards

**IEC61508** – "Functional safety of electrical/electronic/programmable electronic safety-related systems"

This is the "basic safety standard" from which others are derived.

IEC61511 is a version of IEC61508 which has been <u>simplified</u> for the process industries

IEC62061
Machinery Safety
IEC61511
The Process Industries

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#### The Legal Status of IEC61511

- o The Health & Safety at Work Act requires you to reduce risk "so far as is reasonably practicable".
- This means you must have systems in place to assess and manage
- o IEC61511 is "Recognised as Good Practice" by the HSE for achieving functional safety.
  - o Its use is not mandatory, but in practice, it is the easiest (only?) way to demonstrate compliance.

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### Safety Instrumented Functions (SIFs)

- o A protection layer whose objective is to achieve or maintain a safe state of the process when a specific dangerous event occurs.
- o Each SIF will have a sensor, a logic solver and a final element.



o These must operate **independently** from the BPCS

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## Safety Instrumented Functions (SIFs)

o Each SIF will have a calculated reliability, called a Safety Integrity Level (SIL)

SIL	Probability of Failure on Demand (PFDavg)		Risk Reduction Factor (RRF)	
	From	From	То	То
1	0.1	0.01	10	100
2	0.01	0.001	100	1,000
3	0.001	0.0001	1,000	10,000
4	0.0001	0.00001	10,000	100,000

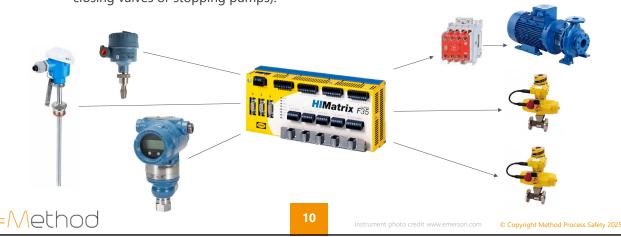
- Works at least 9 times out of 10
- Works at least 99 times out of 100 Etc.....
- o We usually use LOPA (layer of protection analysis) to decide what SIL is required

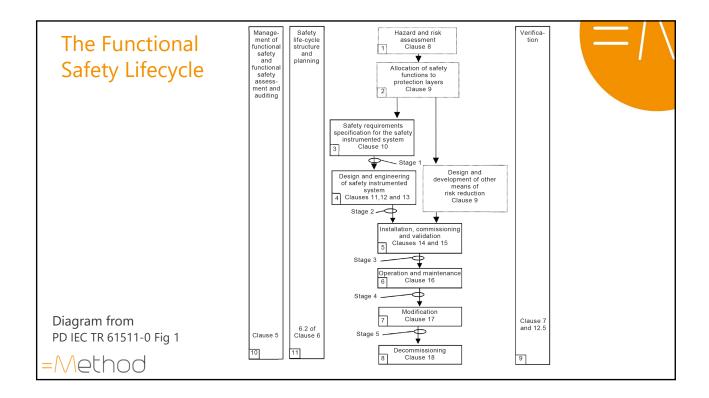
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# Safety Instrumented System (SIS)

- o An independent system, whose function is only to maintain safety.
- A SIS is usually made up of several SIFs
- o The SIS usually remains passive until there is a process upset that the BPCS does not or cannot deal with, and then acts to bring the process to a safe state (e.g. by closing valves or stopping pumps).





#### The Real Basics

- 1) Assess your risks
- 2) Decide what safety functions you need (if any)
- 3) Design and implement them
- 4) Keep them well maintained
- 5) Ensure everything is:
  - Managed well, in accordance with the standard
  - o Done by competent people
  - Checked by competent people





#### The Role of Process Engineers

- o Process engineers have a key role in carrying out hazard & risk assessment (usually using HazOp), and "allocation" (usually using LOPA).
  - o It's usually Process Safety Engineers who lead these studies.
- o Process engineers must work with ECI engineers to define the SIS
  - $\circ$  Our knowledge of process operation and process hazards is vital in getting this right.

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13

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#### The Role of Process Engineers



#### **ECI Engineers' SIF Description:**

"The purpose of this SIF is to close valve X if the temperature goes above 100°C"

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14

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#### **Process Engineers' SIF Description:**

"The purpose of this SIF is to prevent an unventable runaway reaction leading to vessel rupture and up to two fatalities, by closing thermal oil valve X if a malfunction of the BPCS causes the temperature inside the vessel to approach the runaway onset temperature of 120°C"

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15

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#### **Defining Safety Instrumented Functions:**

A useful acronym is "SLATS": **Example:** 

o **S**ensing Measure the reactor temperature using TT01

○ Logic If TT01 > 100°C THEN

• Actuate Close valve x to stop the thermal oil flow

o **T**iming Within 30 seconds

o **S**afety integrity (SIL) And do it to SIL 1 reliability with a PFD of 0.05

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16

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### Some Things to be Aware of



- o Chemical industry SIFs are generally "low demand mode"
  - o i.e. we expect them to operate less than **once** per year.
  - If your SIFs are activating more often than that, it is important that you investigate why and fix the underlying process.

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17

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# Some Things to be Aware of



 HazOp and LOPA are functional safety lifecycle stages, so they need functional safety management (FSM)

To be compliant.....

- o Plan what you're doing in advance
- o Ensure everybody is trained and competent
- o Ensure everything is independently verified (checked)

